

DRAFT

REMEDIAL INVESTIGATION

REPORT VOLUME II

HOOKER/RUCO SITE HICKSVILLE, NEW YORK



PREPARED BY:

LEGGETTE, BRASHEARS & GRAHAM, INC.

APRIL 1990 (REVISED AUGUST 1992)

HKR 001 0294

APPENDIX 1

Detailed Description of Plant Operations

Occidental Chemical Corporation

CERTIFICATION OF ANSWERS TO REQUEST FOR INFORMATION

State of New York County of Niagara

I certify under penalty of law that I have personally examined and am familiar with the information submitted in this document (response to EPA Request for Information) and all documents submitted herewith, and that based on my inquiry of those individuals immediately responsible for obtaining the information, I believe that the submitted information is true, accurate, and complete, and that all documents submitted herewith are complete and authentic unless otherwise indicated. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment.

Thomas L. Jennings

Vice-President
Corporate Environmental Affairs

SIGNATURE

Sworn to before me this 28th

day of <u>Sentender</u>, 1988

Notary Public

SANDRA A. PELLISH
NOTARY PUBLIC, State of New York
Qualified in Miagara County,
Ny Commission Expires 812,899

AFW037

RESPONSE OF OCC TO U.S. EPA CERCLA \$104 INFORMATION REQUEST DATED JULY 11, 1988

BACKGROUND

Over the past few years, a great deal of information has been provided to the New York Department of Environmental Conservation ("NYS DEC"), other state agencies, and the U.S. EPA regarding the operations of the Hicksville Site.

Much of the early interest in the Site was caused by a concern that the Site was a contributor of chlorinated organic chemicals to the area groundwater. This concern was due in part to the reported presence of vinyl chloride in a few water wells near the Site. Since the Company was the only known user of vinyl chloride in the area, the assumption was made that the Company must be the source. It is now known that there can be many sources of vinyl chloride in groundwater.

The reality is as follows. The Hicksville Site is a small site, within and affected by, a large industrial complex. Vinyl chloride has been discovered to be a degradation product of chemicals regionally discarded in large quantities by industrial, commercial and residential users, but discarded by the Company in insignificant quantities. Vinyl chloride becomes a gas at less than 8° F and would not be expected to have reached groundwater in large quantities at the Hicksville Site.

Ubiquitous Regional Use of Solvents

A study performed in Suffolk County traced a plume of vinyl chloride in groundwater to a commercial dry cleaning establishment. The dry cleaner did not use vinyl chloride, but did use perchloroethylene (tetrachloroethylene). solvent was converted either in the dry cleaning operation, or by biologic action in the septic system and groundwater, into vinyl chloride. The perchloroethylene, a common dry was solvent, apparently converted trichloroethylene, then into dichloroethylenes, and finally into vinyl chloride (monochloroethylene). Trichloroethylene was itself a then commonly used metal degreaser and also could degrade to vinyl chloride. The biological degradation tetrachloroethylene and trichloroethylene described in chloride has been "Transformations tetrachloroethene and trichloroethene in Microcosms and Groundwater, F. Parsons, Paul R. Wood and Jack DeMarco, J. Amer. Water Works Assoc. February, 1984 pp. 56-59. A different degradation pathway occurs when solvents are exposed to hot metal surfaces in the presence of water, such as occurs in metal degreasers. This thermal-hydrolytic breakdown of solvents to form vinyl chloride was described in "The Chemistry of Synthetic Resin," C. Ellis, Reinhold Publishing, N.Y., 1935, p. 1035.

Further, through studies reported by the Nassau County Department of Health in 1979 and other government agencies, we now know that a significant source of chemicals in the groundwater on Long Island was the individual consumer use of solvents in septic systems. In Nassau County alone, 76,000 gallons of solvents were introduced directly into the groundwater in 1979 in the form of cesspool cleaning and drain opening products. In a May, 1979 survey performed by Nassau County [Attachment 6], the county estimated a yearly sales volume of 76,000 gallons of organic cesspool cleaning and drain opening products. These included 17,400 gallons per year of methylene chloride; 18,600 gallons per year of 1,1,1-trichloroethane and other halogenated These chemicals were added directly to the groundwater by consumers who poured these solvents into their septic systems. The study was prompted by the discovery of chemicals in wells throughout Long Island. The study lists 11 categories of products and about 230 brands that have the potential to contaminate the groundwater.

The Company did use trichloroethylene, but differently from the typical use of this solvent. The typical use by industrial, commercial (such as automotive garages) residential users was as a degreaser. After use, be discarded. solvent would contrast, In trichloroethylene used by the Company became a component of a product. [Attachment 2 at p. 228, 195] It was not discarded after use and only a trace would appear in any Tetrachloroethylene was an integral process waste water. part of the manufacturing process and it is estimated that less than 40 pounds per year of tetrachloroethylene were discharged to recharge basins [Attachment 2, p. 196]. About year of vinyl chloride pounds per monomer discharged. Even these estimates are biased on the high side because they are based on the higher production years in the late 1970's. It is unlikely that much of the vinyl chloride reached the groundwater, because it boils at 7.9 degrees Fahrenheit and becomes a gas. No chlorinated solvents other than those already discussed were discharged by the Company. [Attachment 2, p. 194 and Attachment 15]

Industrial Neighborhood of Hicksville Site

The Hicksville Site is a 14-acre site in the midst of a thousand acre industrial area. Its largest neighbor occupies or occupied property on three sides of the

Hicksville Site. The <u>Industrial Chemical Survey</u> (NYS DEC 1981) reported that this neighbor had used 1,377,457 pounds of trichloroethylene and 281,288 pounds of tetrachloroethylene annually since 1971. [Attachment 11] Nassau County estimated that the same neighbor used 53 percent of the trichloroethylene used by industry in 1978 in Nassau County. The Company's Ruco Division also used trichloroethylene, but it was incorporated in a product and not discarded. Its use, estimated at 170,000 pounds per year, had ended by mid-1975.

Site Investigations

The Company has extensively studied the Hicksville Site. This study, beginning in 1983, involved the installation of 12 monitor wells at six locations on the Site, the collection and analysis of two rounds of groundwater samples from the wells, and collection and analysis of more than 80 samples from an area at and around a 6 foot by 6 foot area where PCBs were apparently spilled. some trace contamination of groundwater Although detectable on-site, the available data shows that trace contamination may originate to the east on the property of a Site neighbor as well as upgradient to the north from other As noted this neighbor occupies or occupied sources. property on three sides of the Site, and there is reason to believe that groundwater flows from its property, onto the Hooker/Ruco Site, then back onto the neighbor's site. Any groundwater flowing back onto the neighbor's site is presumably captured by its pumpage, and treated in its treatment systems. The maps in Attachments 9 and 10 indicate the widespread historical presence of solvents and vinyl chloride in the areas surrounding the Hicksville Site. appear a relationship to show also trichloroethylene and tetrachloroethylene concentrations and vinyl chloride concentrations in groundwater at distance cross radient from the Hicksville Site.

The only significant contamination remaining on-site is PCB residues on soil in a small section of the Site. We believe adequate data is now available to define this contamination, but we have agreed to undertake more sampling as part of the RI/FS which U.S. EPA has determined must be undertaken. The Company was prepared to remediate this area in cooperation with the NYS DEC, when further action was halted by the removal of the NYS DEC as the lead agency by the U.S. EPA.

Estimates of Types and Quantities of Waste

A number of attempts have been made to estimate the types and quantities of waste produced by the Company's Hicksville plant. These efforts started in 1978 and attempted to identify the wastes produced based on then current activities and recollections of on-site personnel. Due to the passage of years, very little information is available today. Thus, this response does not attempt to calculate the number of pounds of an individual chemical which may have been disposed as trace components of wastewater discharged to on-site recharge basins decades ago. Any such calculation would be fiction.

We have, instead, attempted to provide a picture of the overall operations at the Site during the period of Company ownership. You have expressed interest in analyses of effluents which were discharged to the recharge basins. Until the mid-1970's, standard analytical procedures for the determination of specific organic compounds such as vinyl chloride and even the common solvents trichloroethylene, tetrachloroethylene and 1,1,1-trichloroethane at trace levels in water were not available. As a result, sampling results that are available are for the most part conventional parameters such as pH, total suspended solids (TSS), and biological oxygen demand (BOD). We did not believe this type of sampling result would be helpful to you and have not included such information in this response.

Also, the concentrations of Ruco chemicals historically reported in process water greatly overstate the concentrations to be found in the sumps because of the large amount of reactor rinse water and non-contact cooling water reaching the sump in addition to process waste water. This is described below in the section entitled "Water Supply". We would estimate that the comparable concentrations in the sumps would be greatly reduced by this dilution.

Answers to EPA Questions

Numbers and letters in parentheses refer to the questions in your letter. Where sufficient data is not available to respond to your questions, no response is included.

Question 1

(1.b.) The Company president is J. R. Hirl, the Chairman of the Board is R. Irani, and the Chief Executive Officer is R. Irani. Their address is Occidental Chemical

Corporation, Occidental Tower, P.O. Box 809050, Dallas, Texas 75380. (1.c.) The Company is incorporated in New (1.d.) The Company has subsidiaries; however none is a significant operating company in this country and none had any relationship to the Hicksville Site. (1.d.) The parent Occidental Company's ultimate is Petroleum Corporation ("OPC"). The President is R. Irani and the Chairman and Chief Executive Officer is Dr. Armand Hammer. Their address is 10889 Wilshire Boulevard, Los Angeles, CA OPC is incorporated in Delaware. (1.e.) Both the Company and OPC accept service of process through CT Corporation.

Question 2

The Hicksville Plant Site was developed by (2.f.) Rubber Corporation of America, a small privately-held company. (2.b. and 2.c.) Operations at the Site began in included natural rubber latex storage, and concentrating and compounding. Five years later, the plant began producing small volumes of plasticizers. These activities were expanded and modified through the years. (2.d.) In 1965, a polyvinyl chloride plant was built, and initially operated under the name Insular Chemical oration. This plant continued in operation until 1975. Corporation. (2.a.) Hooker Chemical Company purchased Rubber Corporation of America in 1965, and operated the facility as the Ruco Division. (2.d.) Hooker has undergone several name changes, with the current name being Occidental Chemical Company. (2.b. and 2.c.) The Site was sold to employees in February Thus Occidental Chemical Company or the Rubber 1982. Corporation of America owned and operated the Site between 1945 and 1982. The Site is now operated by a privately held corporation under the name (2.f.) Ruco Chemical Corporation which is not affiliated with the Company. (2.e.) Although the Company did not lease any portion of the Site to third parties, the office building for the plant was a leased building north of the Site.

PVC (polyvinyl chloride) was a key material in the products made at the Site. Prior to 1955 this material was purchased from outside sources. In 1956, a partnership was formed with Ross & Roberts of Stratford, Connecticut to construct and operate a PVC production facility at the Hicksville Site. This joint venture was known as Insular Chemical Corporation. Insular was later dissolved when Rubber Corporation of America purchased its partner's share. Today, no distinction is made between the property which was under the control of Insular and the property which was

owned by Rubber Corporation of America. The Site encompasses all of this property.

Through the years in which the Company operated the Site, various processes were employed including the manufacture of polyesters, polyurethanes, and specialty plasticizers for the vinyl industry. As mentioned above, during the period 1956 to 1975, polyvinyl chloride was produced at the Site. Other products included vinyl film and sheeting, solution polyurethanes and polyurethane latexes, dry blends and pelletized plastic compounds. A pilot plant produced polyester, plasticizer and polyurethane products, and the laboratory was utilized for organic chemical synthesis and technical service. [Abramowitz Testimony - Attachment 2]

Question 3. Processes

In the following discussion, each of the production processes is discussed separately.

- (3.c) To provide an insight into the wide variety of raw materials which were used in the Hicksville processes, we have included a copy of a letter to the Nassau County Department of Health dated January 5, 1977 which includes lists of raw materials used at the Site from 1970 to 1976. [Attachment 7 Raw Material Lists.]
- (3.f) Process flow sheets are attached [Attachment 8] for monoester, polyester, polyurethane, and latex production. A similar flow sheet was not available for PVC.

Where responses are incomplete, the lack of information is primarily due to the detail requested. Due to the passage of years, little information remains on the details of production.

3.a. Latex and Latex Compounding

This process operated from 1945 to 1971. (3.c.) The process involved the co-polymerization of styrene and butadiene under pressure, in the presence of water, in a reactor with the aid of catalysts, additives, heat and agitation. The resultant product was a milky liquid, known as a latex. This latex product was sold as-is to other manufacturers for final use, or was further concentrated and modified by the Company. In the concentration process, the latex was circulated under heat and vacuum to gently remove water. Latex compounds were made by dispersing additives such as pigments and fillers into the raw latex to provide

special characteristics desired by the customer. Latex is considered non-hazardous, and is used in the manufacture of surgical gloves and other rubber goods. It is also the base for the manufacture of chewing gum and is used in the manufacture of adhesives. (3.b.) Production of latex is estimated to have been about 40,000 pounds per week.

There were only two wastes from the process, one a The solid waste was dried solid and the other aqueous. latex rubber which was generated by the drying of spilled latex or by the peeling of dried latex rubber from equipment during cleaning operations. About 300 pounds per week of This waste is non-hazardous and this waste were produced. was added to the plant trash for off-site sanitary disposal. liquid waste was generated from a (3.j.)The stripping operation and from periodic flushing of equipment. from the vacuum stripping contained small water quantities of styrene and butadiene. This water was routed outdoor recharge basins, along with the reactor flushings. These latex wastes are regarded as harmless.

Periodically, the recharge basin bottom was scraped, and these scrapings, containing a mixture of soil and coagulated rubber, were sent off-site for landfilling. When the latex operations were closed in 1971, the recharge basin was drained.

In 1970 a 10,000 gallon outdoor storage tank of styrene (nearly full) polymerized to a solid mass. After the reaction cooled, the tank was completely solidified with polystyrene, the plastic used to make clear plastic drinking cups and the material used in making foamed plastic coffee cups. This tank was sent off-site for disposal.

3.a. Esterification

In 1950, the Company began making small quantities of (plasticizers). Polyesters were added as a These were manufactured in jacketed product line in 1959. reactors equipped with agitation and condensers. These esters were made by reacting organic acids, such as adipic acid with alcohols or glycols, such as octyl alcohol or ethylene glycol with the help of heat and a catalyst. Water was a by-product which was removed to allow the In some products, reaction to proceed to completion. perchloroethylene was added as an inert carrier for this This water was removed by vacuum water of esterification. distillation. The perchloroethylene and water carried over some of the reactants, such as the alcohols or glycols. the case of plasticizer production, an excess of alcohol was used to facilitate water removal from the product. This recovered material was saved for recycling to the following batch. Over the years, trimellitate plasticizers, maleate esters, fumarate esters, and more recently, polyesters were made. Caprylates and pelargonates were also made.

Wastes from the process included both solids and ds. Decolorizing carbon was added during plasticizer liquids. manufacturing to reduce color formation. This carbon was removed from the product by filtration through a filter The filter cake removed from the press was sent press. (3.j.) Liquid wastes, including off-site for disposal. water with dissolved organic acids, alcohols and glycols were originally sent to an outside recharge basin. 1975 on, these wastes were incinerated on-site under permit from New York State. (3.b. and 3.d.) In 1978, at a production rate of 26 million pounds per year, the plant was incinerating about 4,000 gallons per day of waste water (around 12 million pounds per year.) This is the highest production rate experienced in any previous year. This wastewater stream contained one to ten percent of mixed glycols and alcohols. The wastewater stream also contained perchloroethylene (with an estimated discharge of about 40 pounds annually), at times methanol, and also organic acids such as adipic, trimellitic, phthalic, and isophthalic. Some of these materials have other very common uses, such as adipic acid which is an FDA approved food acidulant, and ethylene glycol which is used in anti-freeze. Non-aqueous were sent off-site for disposal, either by landfilling or incineration.

(3.b.) the Company's ester production increased from small initial quantities of perhaps one million pounds in 1950 to about 26 million pounds in 1978.

3.a. Vinyl Film & Sheeting

(3.c.) In this process, PVC resin was blended with plasticizers, pigments, stabilizers and other additives prior to hot mixing and feeding to a calender. A calender is a series of large, heated metal rolls between which the molten plastic mass is fed through increasingly smaller clearances, until a film or sheet of the desired thickness is formed. The hot sheet is finally peeled from the last roll and passed over a series of cooling rolls before reaching a wind-up station. The only wastes generated in this process were scraps of plastic and floor—sweepings. These harmless plastic pieces were added to the plant trash for off-site disposal. There were no liquid wastes from this process. (3.a.) The calendering operation at the Site

started in 1952 and ceased operation in 1969. (3.b.) Annual production was about 7 million pounds per year.

3.a. PVC Resins

The Company manufactured PVC resins by a well known suspension process of polymerization. (3.c.) The primary raw material for this process was vinyl chloride monomer, a material which is a gas at atmospheric temperatures and Under pressure, or refrigeration below 7 9 pressures. degrees Fahrenheit, the monomer becomes a liquid. monomer was received in rail cars, and was fed into jacketed reactors under pressure, along with water, suspending agents (soaps), buffers, and catalyst. In the agitated reactors, under pressure, and somewhat elevated temperature, the vinyl chloride was converted to polyvinyl chloride resin in a Whereas the monomer is a gas under slurry with water. atmospheric conditions, the polymer is a solid white powder. Although the process initially requires heat to start the reaction, as the reaction proceeds, cooling is required to This cooling was provided by control the temperature. circulating non-contact water through the reactor jacket. The reaction was usually allowed to proceed to 90 to 95 percent of completion, after which the unreacted monomer was stripped from the batch in a separate stripping vessel, condensed and recovered for recycling. The stripped resin slurry was then centrifuged to remove most of the water, and was finally sent through a rotary dryer to remove the remaining moisture. (3.c.) Some products required the addition of vinyl acetate to the reactor to produce a co-polymer of vinyl chloride and vinyl acetate. The basic process was similar, but vinyl acetate was added to the reaction mixture, and the catalyst and additives were adjusted.

(3.a. and 3.b) Starting in 1956, the facility operated at an average rate of 9 million pounds of product per year. The process was shut down in 1975.

Wastes from this process consisted mainly of aqueous effluent from the centrifuge and rinse water from the reactors. (3.j.) These wastes were discharged to outdoor recharge basins. (3.e.) Each year, about two million gallons of process wastewater were discharged to the recharge basins. Leaving the process, the wastewater stream probably contained 600 to 1,200 parts per million of dissolved organics. Included in the dissolved organics were trace levels of unreacted monomer. A former plant employee estimated that the total level of monomer in the wastewater was about two to three parts per million. [Attachment 1,

Abramowitz letter, June 5, 1979.] Since the individual formulations varied, so did the ratio of components in the wastewater. A breakdown of contaminants based on a typical copolymer formulation may be two to three parts per million vinyl chloride, 100 to 175 parts per million gelatin, 100 to per million methocel (a soluble form 175 parts cellulose), 50 to 100 parts per million barium-cadmium stabilizer, a trace of trichloroethylene and lauric acid, about 100 parts per million of sodium acetate/bicarbonate, and 250 to 650 parts per million of vinyl acetate. The barium and cadmium soaps were in use only for a short period of the plant operation. Only during this period would traces of these materials have been present in The 2 to 3 parts per million VCM is the wastewater. equivalent of about 50 pounds per year. (2 million gallons x 8.33 pounds per gallon x 3 parts per million = 49.98 pounds.)

An important point is that, in addition to the 2 million gallons of process water, an equal quantity of relatively clean reactor rinse water was discharged. Also, non-contact cooling water was used. Thus, the actual concentration of materials reaching the groundwater would be much less than the above estimates for process water.

In addition to the dissolved organics the wastewater contained very finely divided particles of PVC which were too small to be captured by the centrifuge. In the recharge basins, the PVC settled out, and most of the vinyl chloride evaporated into the atmosphere due to its high volatility. About once per year, the recharge basin bottoms were scraped, and these scrapings, primarily containing PVC resins, were removed for off-site landfill disposal. The PVC operation ceased in 1975.

3.a. Polyurethanes

These products were manufactured either in 55-gallon drums or in temperature controlled reactors. (3.a.) Small scale production began in 1962. (3.c.) Raw materials were normally polyesters, a di-isocyanate, glycol-type chain extenders, and a catalyst. Solvents, such as toluene and dimethyl formamide (DMF), were added to keep the final product in a fluid condition. Temperature control was essential for product quality and uniformity, and the process took place under constant agitation. The final product was a high molecular weight polyurethane resin in solvent solution. (3.e.) Water was not used in this process other than as non-contact steam or cooling water.

Two types of liquid wastes were produced in the process. Non-halogenated solvents, such as toluene, were used periodically to flush the reactors to provide clean reactors for product changes. These flushings were sent off-site for incineration. The second type of waste was off-specification product. If the product could not meet specifications, it was sent off-site for landfill disposal.

3.a. Vinyl Compounds

Two basic types of vinyl compounds were manufactured by the Company at the Hicksville Site, dry blends and pellets. (3.c.) In either case, about 90 percent of the formulation was PVC resin, with the remainder being such additives as pigments, lubricants, heat stabilizers and impact modifiers. (3.a.) The compounding operations started in 1958. The dry blends were made by placing this mixture in a high speed blender, and mixing vigorously for a few minutes. The friction of the mixing caused a heat build-up, so the mixture would then be quickly discharged to a cooler to prevent decomposition. This product was then suitable for some uses, such as the manufacture of vinyl phonograph records. Other uses required the formation of pellets, so the dry blend was fed through an extruder, which melted the material, and forced it through a die with a rotating knife at its face to produce a pelletized product. This type of product was used for the manufacture of clear plastic bottles and blister packaging. (3.e.) Water was not used in this process.

Waste from the compounding process was mostly paper sacks in which the raw material arrived, and some floor sweepings. In the early days of plant operation, the paper bags were bundled and sent off-site along with the floor sweepings for municipal landfilling. Later, the bags were compacted and sent to a secure landfill, along with the floor sweepings. There were no liquid wastes from this process.

Question 3.g, 3.i, 3.j

It is our belief that the wastewater disposed of on-site in the recharge basins was not and is not hazardous due to either the innocuous nature of the components or the low concentration of those materials which today may be considered hazardous. Of those chemicals now listed as hazardous substances pursuant to CERCLA \$101(14), only the following would have been found in the Company's waste at various times and not necessarily above reportable quantities: adipic acid, barium, cadmium, methanol,

methylethylketone, phthalate esters, phthalic anhydride, polychlorobiphenyls (PCBs), styrene (but not polystyrene), tetrachloroethylene, toluene, trichloroethylene, urethane (but not polyurethane), vinyl acetate monomer (but not polyvinyl acetate), vinyl chloride monomer (but not polyvinyl chloride).

We have not included information relating to off-site disposal as the thrust of your inquiry is related to the RI/FS at the Hicksville Site which is being conducted by the Company pursuant to a Consent Order with U.S. EPA.

Reference should also be made to responses above in Question 3.

Question 4. On-site Waste Storage/Disposal

Latex solidified in three storage tanks and these tanks could no longer be used. In 1974 these tanks were removed from Plant 1 and were buried at the Site between the parking lot and the railroad right-of-way. These tanks were filled with sand and covered. The latex is not considered hazardous.

In the latex operation, latex was moved by trailer from Plant 2 to Plant 1 where it was concentrated. In time, the trailer would become encrusted internally with solid latex rubber, and the tank trailer would be discarded. In approximately 1962 a trailer was buried on the property between the Plant 2 solvent tank farm and the PVC catalyst cold room. Plant personnel believe that a second trailer was shipped off-site for disposal.

Reference should also be made to the answer to Question 6.

Question 5. Spills and Releases from Processes

In 1978 the plant was using 33,000 pounds of Speedi-Dri to soak-up and clean-up chemical spills (plasticizer, 2 - ethylhexanol and other alcohols, polyester, polyurethane, urethane latex and oil spills). Plant personnel estimated that about one-half part of organic was absorbed in each part of Speedi-Dri, thus the amount of spilled material was about 16,000 pounds per year.

Occasionally, ester plant wastes overflowed their concrete sumps (which fed the incinerator) and entered the now inactive Plant 1 Ester Plant Recharge Basin.

For some time, the Pilot Plant hot oil system used oil containing PCBs. Periodically, the system had upsets in which oil erupted through a relief pipe, ran down the outside of the building, and soaked into the ground. This ground area was believed at the time to be about six feet square. The system was converted to non-PCB oils, and the contaminated area was paved over. This area has been 1983 to define the extent of the PCB studied since The most recent samples were taken on contamination. February 18 through March 18, 1988. The contamination is largely defined at this time. The area The most recent sampling and analysis report was presented to the U.S. EPA on June 23, 1988.

Question 6. Other Spills and Releases

The Company has had occasional spills of raw materials during transfer operations. These spills have been cleaned up, and the clean-up materials have been sent off-site for landfill disposal. One such spill in 1982 was 300 to 500 gallons of isodecyl alcohol which was spilled when a temporary transfer line broke. The spilled material was soaked up with Speedi-Dri and visibly contaminated dirt was removed. Spills such as this were reported to Nassau County as well as the NYS DEC.

Over the period that the ester plant was operating, the bulk truck loading and unloading operations resulted in minor dripping and minor leakage of plasticizer, alcohols, and latex in the ester tank farm area. There were also occasional tank overflows. The area used for the loading/unloading was neither paved nor diked. As a result, the spills could soak into the ground, and under storm conditions, the spills could be washed to the back recharge basin.

Similarly, the area to the west rear of Plant 1 where plasticizer trucks were loaded would have received minor drippings and spillage. This area was not paved, and during storm conditions would have been a source of plasticizer to the back recharge basins.

For a period of time, several hundred drums of wastes were stored on-site in areas both north and south of Plant 2. These were stored until arrangements were made for appropriate off-site disposal. The drums contained such waste as 2-ethyl hexanol, other alcohols, perchloroethylene, solution urethane, solvents such as dimethyl formamide, toluene, methyl ethyl ketone, isopropyl alcohol, waste plasticizer, waste polyester, and filter cakes. Due the

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long storage time, some of the drums rusted through, allowing the contents to be released to the ground. The drums were removed and sent for disposal off-site. Soil contamination remaining may have resulted in stormwater contamination. This stormwater would discharge to the Pilot Plant Recharge Basin.

Question 7. Pilot Plant & Laboratory Processes

The laboratory was used for a wide variety of process research and quality control functions associated with the plant operations. Wastes and effluents from the laboratory were minimal.

Laboratory and pilot plant synthesis processes and the chemicals they emloyed were essentially small scale versions of the plant manufacturing operations. There was a pilot scale hot oil system in the Pilot Plant. Periodically this system had upsets in which PCBs were released. This is discussed in the answer to Question 5.

Question 8. Storage Tank Leak Tests

On review of our files, we could find no information regarding tank leak tests. A listing of all storage tanks, capacities, materials stored in each tank, and how they are handled was submitted to the Nassau County Department of Health as part of the Site Spill Control Plan. [Attachment 3-Letter: P.B. DeVries to Nassau County Department of Health, April 29, 1981.]

Question 9. Lagoons/Septic Tanks

Although no septic tanks are in use at the Site today, at the time of Company ownership, there were five septic tanks in use. These septic tanks were used only for sanitary wastes. They were permitted to discharge a total of 4,000 gallons per day to the groundwater. [Attachment 4 - 1981 Underground Injection Control Questionaire.] There were and are no lagoons on the Site. References should be made to Question 13 relating to recharge basins.

Question 10. Water Supply

Originally, the Company water supply was primarily from on-site wells. These wells have now been shut down, and water is supplied from City mains. Company pumpage during the period January 1960 to January 1969 (a period for which records were available) averaged about 95,000 gallons per day. In 1958, these wells were permitted to pump 600,000

gallons per day, with a maximum of 120 million gallons in one year. In 1960, the pumpage was about 330,000 gallons per day. As the wells were taken out of service, this dwindled to about 35,000 gallons per day in 1968. One by one, the wells were shut down because of clogging from a build-up of naturally occurring iron bacteria. These wells were N5368 installed in May, 1955; and well N3450 installed in March of 1950, rebuilt in October, 1955 and shut down in July, 1960; and N5390 installed in October 1955 and shut down in June 1965. Occasional well use continued until October 1970, however. [Logs of these wells are included as Attachment 5.]

Question 11. Plan of Site

The U.S. EPA and their contractor, EBASCO, have been provided with drawings of the Site.

Question 12. Production and Monitoring Wells

The original water supply for the Site was primarily from on-site wells. These wells were N5368 installed in May, 1955; and well N3450 installed in March, 1950 and rebuilt in October 1955; and N5390, installed in October 1955. [Logs of these wells are included as Attachment 5.] Company pumpage during the period January 1960 to January 1969 (a period for which records were available) averaged about 95,000 gallons per day. In a 1964 form submitted to the Nassau County Department of Health, the pumpage was estimated to be from 68,400 to 102,600 gallons per day [Attachment 14]. In 1958 these wells were permitted to withdraw 600,000 gallons per day. These wells were in operation at various rates of withdrawal from 1950 to 1970. After this time they were shut down because of clogging from a build-up of naturally occurring iron bacteria.

Twelve monitoring wells were installed in two well clusters at six locations on the Site in 1983. Well logs and construction details have been provided to the U.S. EPA. The first set of groundwater samples were obtained from January 30 to February 7, 1984. A second set of groundwater samples were obtained during the period from May 6 to May 10, 1985. The results of this sampling and analysis were reported in a February 1986 report entitled "Report of Groundwater & Soils Investigation at The Former Ruco Division Plant Site, Hicksville, New York. This report has been given to the U.S. EPA.

Question 13: Recharge Basins

During the early days of plant operations, recharge basins were used for the treatment/disposal of all plant effluents, including PVC production effluents, effluents operation, and the latex effluents from manufacturing. These discharges took place under New York SPDES Permit. The latex operation ceased in 1971, at which time its basin was drained and cleaned out. The on-site incinerator for ester wastes came online in early 1975, eliminating the discharge of ester wastewater to the ground. Following the PVC process shutdown in 1975, the recharge basins received only stormwater. Each of these is described further below.

You have expressed interest in analyses of effluents which were discharged to the recharge basins. Until the mid 1970s, standard analytical procedures for the determination of specific organic compounds such as vinyl chloride and the common solvents trichloroethylene, (perchloroethylene) tetrachloroethylene and 1,1,1trichloroethane were not available. As a result, sampling are available are for the most conventional parameters such as pH, total suspended solids (TSS), and biological oxygen demand (BOD). We did not believe this type of sampling result would be helpful to you, and have not included such information in this response.

PVC, Vinyl Chloride/Vinyl Acetate Copolymer, and Latex Recharge Basins - Plant 2:

In 1956, the Company went on-stream with a PVC resin facility making both PVC (polyvinyl chloride) and vinyl chloride/vinyl acetate copolmyer. Production rate of this suspension plant was about 10 million pounds per year. Approximately two million gallons of process wastewater were discharged annually to the Plant 2 Recharge Basins. This wastewater contained about 0.1 percent PVC resin solids (too fine to be collected by the process centrifuge), and contained 600 to 1,200 parts per million dissolved organics. Included in the dissolved organics were trace levels of unreacted monomer. A former plant employee estimates that the total level of monomer in the wastewater was about two to three parts per million. [Attachment 1] This is the equivalent of about 50 pounds of vinyl chloride per year. Since the individual formulations varied, so did the ratio components in the wastewater. breakdown of A contaminants based on a typical copolymer formulation may be two to three parts per million vinyl chloride, 100 to 175

parts per million gelatin, 100 to 175 parts per million barium-cadmium stabilizer, a trace of trichloroethylene and about 100 parts per million of lauric acid, acetate/bicarbonate, and 250 to 650 parts per million of vinyl acetate. The barium and cadmium soaps were in use only for a short period of the plant operation. Only during this period, would traces of these materials have been in the wastewater. approximately After present production batches, the reactors needed to be entered and manually cleaned due to the build-up of product on the Before and after this cleaning the reactors were walls. The amount of this rinse water was about 2 million rinsed. gallons per year and would dilute the concentrations described above upon entering the recharge basins. water was sent to the Plant 2 recharge basins.

In addition, recharge basins for Plant 2 received wastewater from a vacuum stripping operation used in latex processing between 1956 and 1975. The wastewater probably contained some styrene and lesser amounts of butadiene. Also, rosin acid soaps may have entered the recharge basins during plant upsets.

Ester Plant Recharge Basin - Plant 1:

From 1951 to 1974, process waste from ester production was fed to the Ester Plant Recharge Basin. The ester production gradually increased from five million pounds per year in 1951 to 26 million pounds per year in 1978. In 1978, about 4,000 gallons per day of wastewater were being produced (about 12 million pounds per year). Based on an approximate two percent organic content, the plant in 1978 was disposing of about 250,000 pounds per year of organic waste, which formerly entered the recharge basin. Since 1975, these wastes have been incinerated in an on-site incinerator, and the recharge basin was taken out of service. The basin continued to receive discharges to the floor drains in the Pilot Plant, however. The discharges to the floor drains were apparently stopped late in 1976.

The wastewater that at one time entered the basin contained one to ten percent mixed glycols and alcohols. It also contained organic acids such as adipic, trimellitic, phthalic, and isophthalic. The waste stream also contained small amounts of perchloroethylene and, at times, methanol.

Cooling Tower/Boiler Blowdown and Other \pm Recharged Water:

The plant discharged substantial quantities of water other than process water. In 1978, about 10,800 gallons per day (3,600,000 gallons per year) of cooling tower and boiler blowdown were discharged to the Pilot Plant Recharge Basin. The design flow of these non-contact discharge was listed as 25,000 gallons per day in the May 8, 1975 SPDES application. [Attachment 12] In a July 29, 1977 Nassau County Department of Health Memorandum the cooling tower and boiler blowdown are listed as 10,000 gallons per day each. [Attachment 13] These blowdowns contained low levels of approved boiler and cooling tower treatment chemicals. Before the installation of the cooling tower, much more water was used. As noted previously, the plant was permitted to pump 600,000 gallons per day in 1958, and actual pumpage in 1960 was about 330,000 gallons per day. Most of this water was non-contact cooling water discharged to the recharge basins.

During the period 1956 to 1975, City water was demineralized for use in the Plant 2 PVC and latex processes. Regeneration acids and caustic were discharged to the basin behind Plant 2.

Question 14. Recharge Basin Cleanout

The above discussed recharge basins required periodic cleanout. The materials cleaned from the basins were sent to off-site landfills for disposal. The Plant 2 and Plant 1 basins were cleaned approximately once per year. This material consisted primarily of sand and gravel with resin.

Question 15. Non-insurance Indemnification

There is no non-insurance indemnification.

Ι.

Question 16. Insurance Indemnification

Occidental has maintained series of а insurance programs over the years which would be responsive to its liability at the Hicksville Site, if any. Each such successive insurance programs involved a number of primary and excess coverage layers. The extent of such coverage's responsibility for environmental liabilities, including at is in litigation (Occide et.al v. Hartford Accident is (Occidental Chemical Hicksville, Corporation, and Indemnity Company, et. al, N.Y. Sup. Ct., Erie Co.) Index No. 41009-80).

P. O. BOX 456, RIVER ROAD, BURLINGTON, NEW JERSEY 08016, PHONE (609) 499-2300

June 5, 1979

Wald, Harkrader & Ross 1320 19th St., N.W. Washington, D.C. 20036

Attn: Keith Watson, Esq.

Dear Keith,

We agreed to estimate, for the Sub-Committee, the components in the PVC waste water totaling 600-1200 ppm, as mentioned on p. 11 of the J.B. Harrison document dated 8-18-78. Our best breakdown based on a typical copolymer formulation is as follows:

	PPM
vinyl chloride	2-3
gelatin	100-175
methocel	100-175
barium-cadmium stabilizer	50-100
trichloroethylene	trace
lauric acid	trace
sodium acetate/bicarbonate	100.
vinyl acetate	250-650

approx. total range 600-1200

Yours touly, HOOKER CHEMICAL COMPANY

Raymond J. Abramowitz Technical Director

RJA:bb

cc: J. B. Harrison

M. Whitehead.

J. Ruffing

DE ~ - - - - -

JUN 8 1979

Mooker Ruco ovision

NIW SOUTH MOAD, HICKSVILLE, NEW YORK 11802 PHONE (516) 931-8100 TWX 510-221-1871

> April 29, 1981 Engr. 3928

Nassau County Department of health 240 Old Country Road Mineola, New York 11501

Attention:

Hr. L. Sama, Public Health Engineer

Bureau of Land Resources Management

'Dear Larry:

Attached is a listing of all storage tanks, capacities, materials stored in each tank, and how they are handled. We have included a site map indicating locations of all tanks.

Tanks at location B nos. 14, 15, 16, 17A, 17B, 17C, 18A, 18B, 18C, 19A, 19B, 20A, 20B, 21, 22, tanks 1, 2, and 3 at location F and the separator and receiver at location K are below ground. A total of 14. Seventy-two (72) tanks are above ground.

The information submitted is part of our Spill Control Plan.

PBV/es

enc.

cc: J. B. Harrison

H. Dubec

. B. Devries

Site Engineering Manager

HKR 001 031

EC SMEMICAL CORPORATION

"G" " " " " AL PETROLEÚM CORPORATION

1. PRESENT FACILITIES & OPERATIONS

A. MATERIALS COVERID

1. Listed below are the materials covered by this plan:

MATERIAL	STORAGE V	OLUME
Ethylene Glycol/Propylene Glycol		
Mixture (EPG)	- 5,000	gal.
1,4-Butanediol	5,000	gal.
Dioctyl Adipate (DOA)	20,000	gal.
Normal Octyl-Normal Decyl Tri-Mellitate	5,000	
S-1011-35	5,000	gal.
F-203	: 30,000	gal.
1,6-Hexanediol	11,000	gal.
F-2403	6,000	gal.
F-2401	6,000	gal.
26TM	38,200	gal.
#6 Oil	105,000	gal.
C7C9TM	8,000	gal.
T-10TM	24,000	gal.
#2 0il	34,700	gal.
Alcohols	7,650	gal
Alcohol Strip	6,000	gal.
Ethylene Glycol	20,000	gal.
Diethylene Glycol	20,000	gal.
C7C9 Alcohol	55,000	gal.
2-Ethylhexanol	80,000	gal.
Isopropanol	8,000	gal.
Methyl Ethyl Ketone	6,500	gal.
Toluene	15,000	gal.
Dimethyl formamide	10,000	gal.
Iso-octyl Alcohol	10,000	gal.
Adipic Acid	8,000	ft.3
Process Hold Tanks	8,200	gal.
Strip Hold Tanks	9,000	gal.
Empty Tanks •	56,700	gal.
Incinerator Hold Tank	30,000	gal.
Incinerator Effluent Separator	4,000	gal.
Incinerator Effluent Receiver	16,000	gal.
TOTAL LIQUID STORAGE CAPACITY	664,950	gal.
TOTAL RAW MATERIAL SOLID STORAGE CAPACITY	8,000	ft.3

B. STORAGE TANK LISTING BY LOCATION (SEE ATTACHED MAP)

LOCATION A	•		
Tank No.	Contents	<u>Volume</u>	_
23	Alcohol Strip	2,000 gal.)	Compartmented
24	Alcohol Strip	2,000 gal. >	Tank Car
25	Alcohol Strip	2,000 gal.	•

INCATION A (contd)

Tank No	Contents		Volume
26	Al colol		2,550 gal. (Compartmented 2,550 gal. (Compartmented
27	Alcohol.		2,550 gal. (Compartmented 2,550 gal. (lank Car
28	Alcohol		2,550 gal. lank tar
A	2-Ethylhexanol		10,000 gal.
В	2-Ethylhexanol		10,000 gal. \\
C	Product	-	5,000 gal empty
D	Di-octyl Adipate	_	5.000 yal.
£	Iso-octyl Alcohol		5,000 gal.
· f	Iso-octyl Alcohol		5,000 gal.
G	Alfol 610		10,000 gal.
Н	2-Ethylhexanol	_	10,000 gal.
1	2-Ethylhexanol	•	10,000 gal.
J	2-Ethylhexanol		6 000 == 1 1
K	Product		5,000 gal. Compartmented Tank
L .	Di-octyl Adipate		5,000 gal. Compartmented Tank
M	Di-octyl Adipate	•	5,000 gal. Compartmented tank

Materials in tank numbers 23 through 28 are received from another area of the site via tank truck. Materials in tanks A and B are received in bulk (tank truck), and transported to other plant areas in bulk (tank truck). Materials in tanks C and D are received in bulk (tank truck) from other plant areas and shipped in bulk (tank truck) off the site. Materials in tanks E through J are received in bulk (tank truck). Materials in tanks K, L, and M are received from other plant areas in bulk (tank truck) and are shipped off the site in bulk (tank truck).

LUCATION B

Jank No	Contents	Volume	
14	#6 Uil	30,000	ual.
15	#6 Oil	30,000	
16	Incinerator Hold		gal empty
17A	261M	8,000	gal.)
178	26 TM		gal. / Compartmented
170	C7Cg TM		gal. \ Tank
18A	า เบาัท	8,000	gal.) compared and
188	1101M		(rombarrmented
·18C	TIOTM	8,000	qal. [lank
19A	#2 Oil		gal. 7 Compartmented
19B	#2 Oil		gal. J Tank
20A	#6 Oil		gal. 7 Compartmented
208	#6 0il		gal. J Tank
21	•		gal empty
22 .		5,000	gal empty
Silo 1	Adipic Acid	4,000	
Silo 2	Adipic Acid	4,000	ft ³ - solid

Material in tanks 14 and 15 is received in tank trucks, and shipped to tanks 1 and 2 (Location C) in tank trucks. Material in tank 16 is received by tank truck or internal pipe. Materials in tanks 17 A-C and 18A-C are received by tank truck from other plant areas and shipped off-site in tank trucks. Material in tank 19A-B is received by tank truck and transported to tanks 3 and 4 (Location C) by tank truck. Material in tanks 20A-B is received in tank trucks and transported to tanks 1 and 2 (Location C) in tank trucks. The material in silos 1 and 2 is received by railcar or tank truck.

LUCATION C

Tank No	Contents	Volume
1	Ethylene Glycol	. [ناو 000, د
2	1,4 - Butanedial	5,000 gal.
· 3	261M	5,000 gal.
4	NIM	5,000 gal.
4 A	S-1011-35	5,000 gal.
5	F 2 0 3	10,000 gal.
6	F203	10,000 gal.
7	1,6 - Hexanediol	11,000 gal.
10A .	F2403	6,000 gal.
10B	F2401 .	6,000 gal.
11A	26TM	5,000 gal.
118	26TM	5,000 gal.
12A	F203	5,000 gal.
128	F203	5,000 gal.

Materials in tanks 1 and 2 are received in tank truck and piped to other plant areas. Materials in tanks 3 and 4 are received by tank truck from other plant areas and shipped off-site in tank trucks or drums. Material in tank 4A is received by pipeline from other plant areas and shipped off-site in tank trucks or drums. Materials in tanks 5 and 6 are received by pipeline from other plant areas and shipped off-site in tank trucks or drums. Material in tank 7 is received in tank cars or tank trucks and piped to other plant areas. Material in tanks 11A-B is received from other plant areas in tank trucks and shipped off-site in tank trucks or drums. Materials in tanks 10A-B and 12A-B are received by pipeline from other plant areas and shipped off-site in tank trucks or drums.

LOCALION D

lank No	Contents	<u>Volume</u>
A	Hold lank	1,000 yal.
8	Hold Tank	1,000 yal.
C	Hold Tank	1,000 gal.
D	Hold Tank	1,250 gal.
. F	Hold Tank	1,250 gal.
٠. ٤	Hold Tank	1,350 gal.
G	Hold Tank	1,350 gal.
	Strip Tanks	9,000 gal Total
		(18 ea at 500 gal)

Materials in tanks A through G are received by pipeline from other plant areas and transported to various storage tanks by pipeline. Materials in the strip tanks are received by pipeline from other plant areas and transported to other plant areas by pipeline.

LOCATION E

lank No	Contents	Volume
29	Cthylene Clycol	20,000 gal.
30	Diethylene/Propylene Glycol	20,000 gal.

Materials in tanks 29 and 30 are received by tankcar and tank truck and transported to other plant areas by pipeline.

LUCATION F

Tank No	Contents	Volume
1	#6 Oil	10,000 ys1.
2	#6 Oil	10,000 gal.
3	#2 Oil	3,000 gal.

· Materials are received in tank trucks and transported to other plant areas by pipeline.

1 OCATION C

lank No	Contents	Volume
202	261M	12,200 gal.
203		12,200 gal - empty
6		5,000 gal empty
7		5,000 gal empty
10	•	12,500 galempty

Materials in tanks 202 and 203 are received by pipeline from other plant areas and shipped off-site in tank cars or tank trucks; or are transported to storage tanks by pipeline.

LUCATION H

Tank No	Contents	Volume
31 32	2-Ethylhexanol 2-Ethylhexanol	30,000 gal. 25,000 gal.
33	2-Ethylhexanol Isopropanol Methyl Ethyl Ketone Toluene	25,000 gal. 8,000 gal. 6,500 gal. Compartmented Tank
•••	Dimethylformamide	15,000 gal. 10,000 gal.

materials are reveived in tank trucks and transported to other plant areas by pipeline.

LUCATION 1

lank No

Contents

#2 0il

<u>Volume</u>

3,700 gal.

Material is received by tank truck and transported to other replant areas by pipeline.

LUCATION J

lank No

Contents

<u>Volume</u>

2,000 gal. - empty

LOCATION K

Tank No.	Contents	Volume
Effluent Separator	Effluent	4,000 gal.
Effluent Receiver	Effluent	16,000 gal.

Effluent separator is an open top concrete tank designed to separate solids from incineratorable effluent.

Effluent receiver is an open top compartmented (4) concrete tank used to collect and store effluent prior to incineration. One compartment is agitated, and from this compartment effluent is pumped to the incinerator.

ENVIRONMENTAL ACTION INPUT SHEET

=olio: _62707 _(s) Date Entered: _6/19/81 _(e) Agency:N.Y. STATE DEC(25)	
'ndustry Group: P&CS (4) Division: FAB. PDTS. Hicksville, NY 11802 (20)	
Type of Folio: Request for information (20) Number of Items Included: 1 (4)	
Notice Date: _ <u>6/9/81</u> _ (s) Thru:(s) Date Alleged Occur:(6) Thru:(6)	. ,
Date of Next Action:(6)	
Allegation:	(55)
Action Requied: Request for information (underground injection control)	(65
	(55
Current Status:	(55)
	(55)
Penalty Propsd:(20)	4
Disposition When Closed:	(46)
Net Payment:(9) Cost of Corrective Action:(9)	
Date of Completion of Corrective Action:(6) Date Closed:(6)	
Comments:	(55)
Contact Name: Philip B. DeVries (20) Contact Tel. No.: (516) 931-8100 (10)	

_ hooker auco avision

W SOUTH HUAD, HICKSVILLE, NEW YORK 11802 PHONE (516) 931-8100

June 19, 1981

Mr. Dan Meszler
New York State Dept. of Environ. Conservation
Bureau of Permits & Compliance
50 Wolf Road - Room 201
Albany, NY 12233

Dear Mr. Meszler:

Attached Underground Injection Control Questionnaire for the Hicksville facility, Hooker Chemicals & Plastics Corporation, is forwarded in compliance with your request.

As per your conversation with John Hanna of Whiteman, Osterman & Hanna, we have not included any sump that is shallower than its largest surface dimension.

Very truly yours,

Philip B. DeVries Plant Engineer

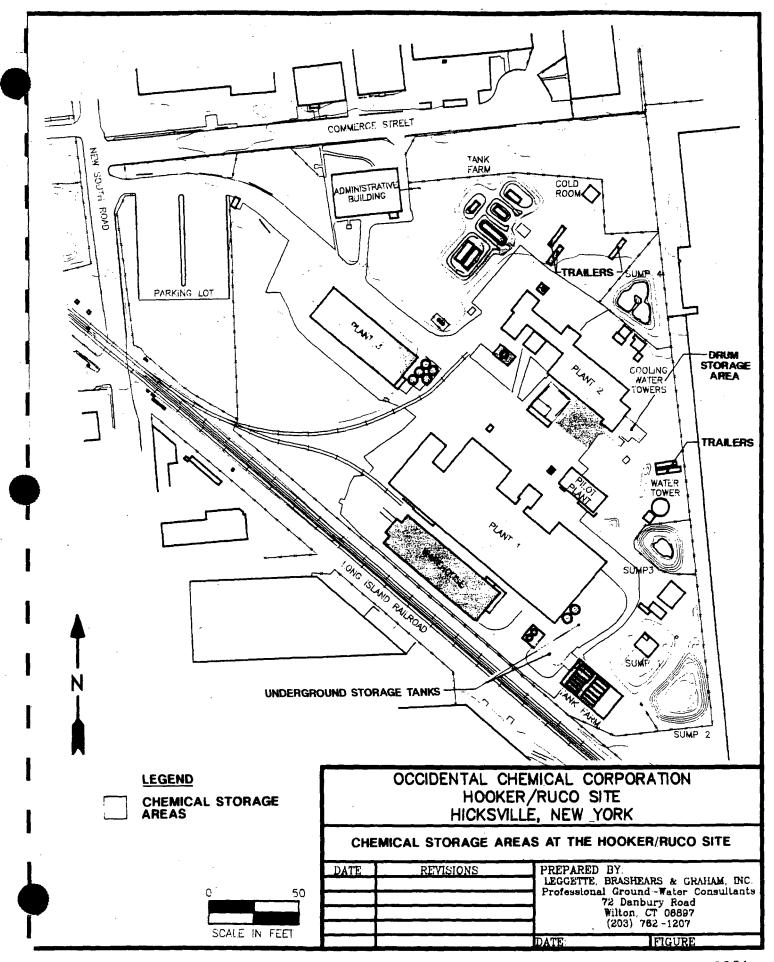
PBD:sg/engr. 3965

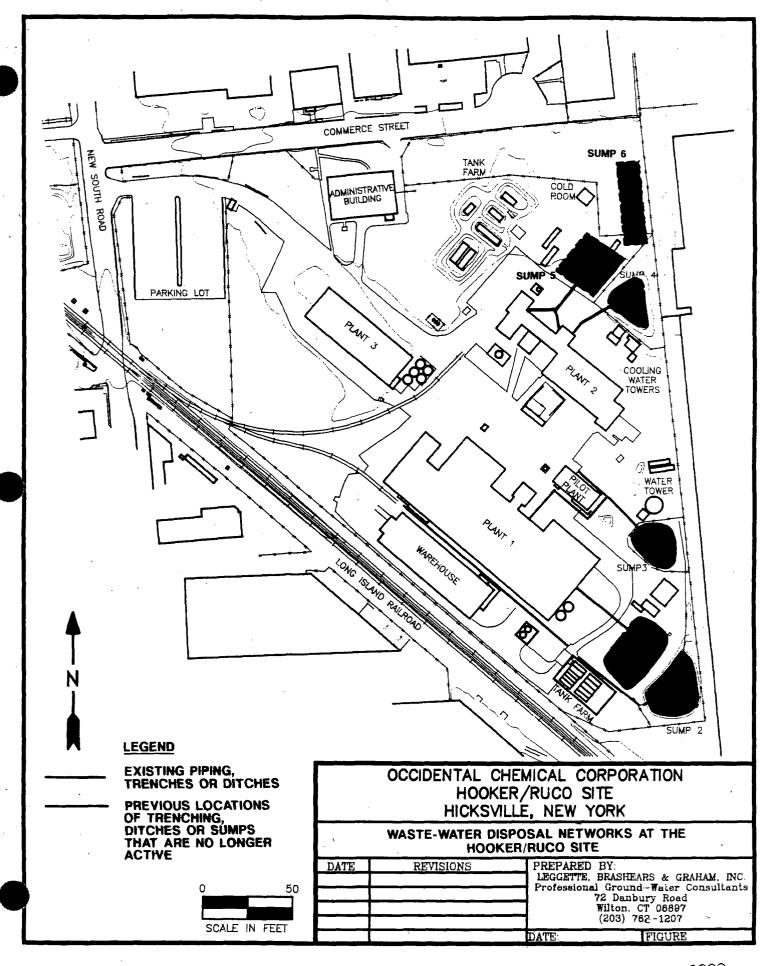
Attachments

CERTFIED MAIL
RECEIPT REQUESTED

bc: J.B. Harrison G. Dubec A. Katona

John Hanna





(U.I.C.) Program

					2		
HOOKEI	R CHEMICALS & PLASTICS COR	æ.					
New Sc	outh Road	•	, 1		• • •		
Hicksy	ville		NY		Nassau	ZIF	11802
TYPE OF C	OWNERSHIP (check one)				· · · · · · · · · · · · · · · · · · ·		
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DESCRIBE	NATURE OF BUSINESS		·				
Manufactu	re of Specialty Polymers	and che	emicals fo	r the	plastics indus	try.	
•					<u> </u>	 	
				·			
	OPERATORS NAME AND AD	DRESS		· 	•		
JERS NAME:	HOOKER CHEMICALS & PLASTI	CS COR	·		·	·	
LET ADRESS:	New South Road				•		
Y:	Hicksville		STATE:	rk	COUNTY: Nassau	216	1180
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APPENDIX A

DISCHAR	iE INF	ORMA	ALIUN
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CHARGE NUMBER TYPE AND SAME FOR FILID OF WASTE BEING DECEMBED

002 per SPDES permit Sanitary Wastes from Plant

FALL SUBSTANCES CONTAINED IN INSCHANGED FLUID OH WAS IL WHICH ARE PRESENT AS A RESULT OF YOUR OPERATIONS, ACTIVITIES OF THE ASSES AND INDICATE THE AVERAGE CONCENTRATION (IN MIGHT) AND THE AMOUNT GENERATED (IN KIGMO*) FOR EACH

None (apparent sanitary waste)

1 31210	S ON PARALITY. T	1			INCHIE	al use of dis	CHAI	TGE	FAC	ALIT	Y (M	ouse	e, disj	2058	etc	ij					
वास	P (4)	D		GE ACI GE		Disposal		-	-				•				,				
E I	YPE AND DESCRIP	TION C	of Discha	MG	FACILITY	finclude depti	and	late	rai d	ieme	melo	na, d	leeign	Now	, act	ual flow, etc.	F				
•	5 septic ta	nks,	appro	×1ı	nate d	imensions	[2 [2 [1	-	5' 6' 4'	- -	0" 0" 6"	X X di	10' 10' a.	-	0" 0"	lateral lateral lateral	ly ly ly	& & &	6' 6' 12'	deep deep deep	;
.,	Total Design		OW OW	-	4,000 3,000	gallons/ gallons/	day day					,	4								

Milligrams per liter

Kilograms per month during an average month

UC-Under construction

E-Existing

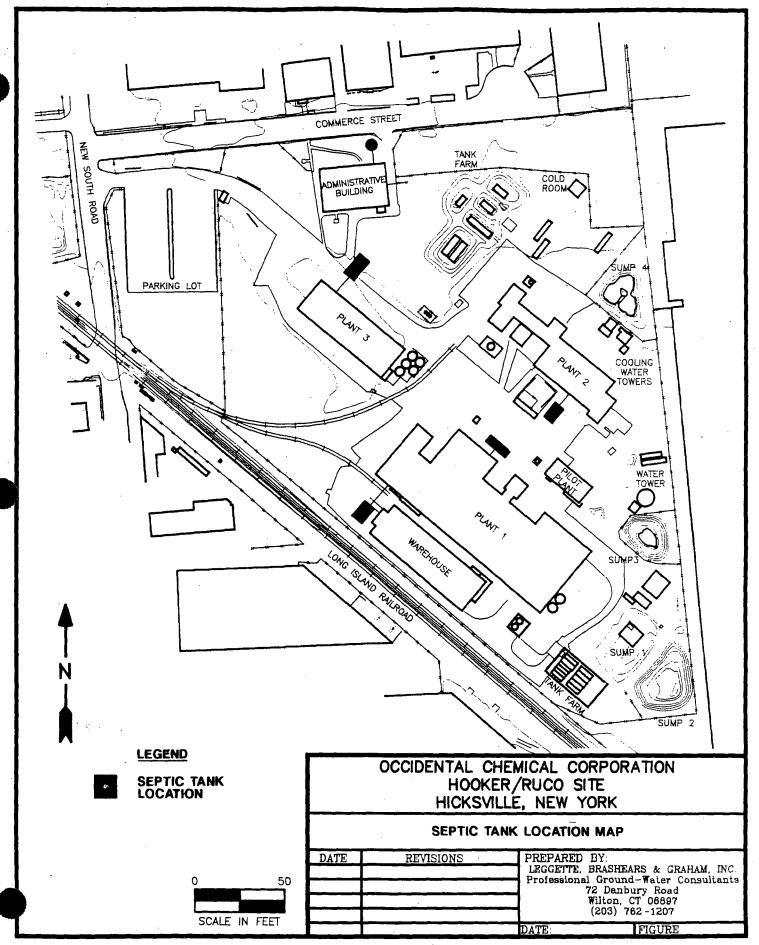
P-Proposed

TA-Temporarily abandoned (indicate date and expected length of abandonment in space above boxes.)

PA-Permanently abandoned and approved by the State (give date)

AN-Permanently abandoned and not approved by the State (give date.)

IF ENOUGH DISCHARGE INFORMATION SHEETS ARE NOT PROVIDED, PLEASE MAKE COPIES SO THAT EVERY DISCHARGE IS REPORTED



PHONE (516) 931-8100

Jan. 5, 1977

Mr. John F. Welsch Nassau County Department of Health Bureau of Water Pollution Control 240 Old Country Road Mineola, N.Y. 11501

Dear Mr. Welsch:

On 11/29/76 you wrote our Mr. Philip DeVries, requesting an update list of chemicals purchased and used by Hooker at the Hicksville plant. You requested this information in the form of an update, and also over the last seven years.

In response to your request, we are supplying you with lists of chemicals purchased and used at Hicksville as follows:

- a. Raw materials used by the Chemicals & Plastics Group RUCO Division, Hicksville, 1970,
- b. Raw Material Requirement, Hooker Chemical/RUCO Division, Hicksville plant, calendar year 1971,
- c. Raw Material Requirement, Hooker Chemical/RUCO Division, Hicksville plant, calendar year 1972,
- Raw Material Requirement, Hooker Chemical/RUCO Division, Hicksville plant, calendar year 1973,
- e. Raw Material Requirement, Hooker Chemical/RUCO Division, Chemical Business Area, calendar year 1974,
- f. Raw Material Requirement, Hooker Chemical/RUCO Division, Chemical Business Area, calendar year 1975,
- Raw Material Requirement, Hooker Chemical/RUCO Division, Chemical Business Area, calendar year 1976,
- Hicksville Dry Blends plant, Raw Materials Used 1973, 1974, 1975, 1976.

Sincerely yours,

J.B. Harrison

Plant Manager

Enclosures sg/MA-3089-7

MICASTUT DET STEMET TEATE RAS MATARIANS USED 1973, 1974, 1975, 1976

RAW MADERIAL DESCRIPTION:

DR AVI 47 Mark 200 Mark 1500

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3158 (charge Serin (Clib)
B-255 6(40) Resin
8-221 Ribay Resin
H-303 FULL Resin
Irrigol 53? Resia
Kane Ace 522
Aldo 18. (General 6000)
Boescht San L
Glycolube FC
2t Zirs Toner
181 8074 (Sympton 1011, 1M 180)
Barium Steamite (Sympton 160)
Acreses C
Raven 1035 (Regal 300, N219, 999 Powder, Superha)
K 120 NO
K 120 N (Supercry1 100)
Ti n
Calcium Stearate
XL 165 (Rosswax 165, Aristocax 165)
AC 629A
K 125
Conditte 95 T
Adjust Tink
Ocaybsh
T-31
T-21)
Poly Flo PVN
CC 7500
CC 10
KM 229
Rhodoriol
Killie Ace P1 20
Vinylube 36
Synpron 1337
Drapez 6.8
LOD
Lubroi TSC
Irvino 340 & 640 Resin
B-202 Resin (Temeco 10R)
Glycolistic 200
Gron 65-1
W
Sympton 1135
Timevin P
M 52 18
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177 001 00

Therm 813 Theres: 531 Proceed 2201 Continues Mark 327 340 - 1 5311- 1 651 Rutile 31 Black D Toner B6 161 P G-62 (Vikoflex 7170) Cateion Line Fener Mark 996 Mark 1800 11 2irs Staurone D1005 Irvinol 659 (Pti 3614 Cab-O-Sil Tiffare R. 101 KM 229 T 1116 Advawax 140 B-342 Resin K-21442 Esceflex 150 Nyostah V982 Mark 292 Mark 583 8-28 Resin Synpron 768 Cologon Al FDA Tonor Dim Mark as Murk C Stearie Acid R-341 Kesin EP-8 EP-0 Drapex 1.4 Ultra Marine Slac ध्यः । ।।।। PFR 100 Fintote Plast. Staffex 626 VC-111 nio:

RUCO DIVISION

17 10161 11/

1470

Raw Material Description

```
them 233 2-Ethyl Hexanol
them 1002 Perchlorethylene
them 1003 Philiplic Anhydride
them 1004 Iso Octyl Alcohol
Them 1008 Adipic Acid
them 1010 Butyl, Alcohol
them 1015 Tricthylene G
them 1015 Triethylene Glycol
them 1022 Iso Decyl Alcohol
them 1032 Funntic Acid
Them 1033 Maleic Anhydride
them 1055 Tri Decyl Alcohol
them 1060 Ethylene Glycol
Them 1061 1, 4 Butanediol
Chem 1074 Mctliyl Amyl Alcohol
Cham 1093 Methylene 2208
Chem 1094 Kethylene 2209
Chem 1102 Iso Phthalic Acid
Chem 1117 Trimellitic Anhydride
Shem 1120 Hylune IM
Them 1122 Cellulose Acetate Butyrato
Them 1124 Ethyl Acetate
Them 1125 Toluol
Them 1129 Glycol Elend
Them 1138 Azelaic Acid
Them 1145 Alfol 610
Them 1149 Di Hethyl Formamide
Chem 1152 Isopropanol
Chem 1164 Di Iso Butyl
Chem 1177 Groco 6 Ole
         1164 Di Iso Butyl Carbinol
1177 Groco 6 Olcie Acid
Them 2042 1, G Hexane Diol
Them 2043 Iso Butyl Alcohol
Shem 2044 Bultrathane H
Them 2056 Alfol 810
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JOKER CHEMICAL & PLASTICS GROUP

RUCO DIVISION

1970

Raw Material Description

Them 2061 Reopentyl Glycol
Them 2062 Dicthylene Glycol
Them 2074 Hylene W
Them 2083 Hondur TD 80
Them 2209 Methyl Cellosolve
Them 2257 N Propanol
Soil 113 Xylol >
Soil 131 Methyl Ethyl Ketone

RESIN
Them 1 Vinyl Chloride Them 2 Trichlorethylens
Them 8 Vinyl Acetata

LATEX Chem 25 Styrene Chem 26 Butadiene Chem 35 Dresinate 731

pry blend & Pellets
Syn 965 VC-65 Resin
Syn 966 Blacar 384 or VC-113 Resin
Syn 971 VC-95 Resin
Syn 986 VC-80 Resin
Syn 994 Acryloid K 120-N
Syn 998 C-155 Rucon Resin
Syn 1007 Kane Ace B-12
Syn 1008 B-28 Rucon Resin
Syn 1009 B-22 Rucon Resin
Syn 1013 B-20 Rucon Resin
Syn 1016 B-34 Rucon Resin
Syn 1016 B-34 Rucon Resin
Syn 1048 KM-636

OKER CHEMICAL & PLASTICS GROUP

RUCO DIVISION

1970

Raw Haterial Description

DRY BLEND & PELLETS (cont'd.)
Chem 1160 Advawax 140
Chem 2053 Adol RP Glycolule
Chem 2069 H & T 831
Chem 2119 H & T 813
Chem 2020 TM 918+
Chem 2081 RO 37+
Chem 2178 Mark 1197

*HOOKER CHEMICAL/MUCO DIVICION-MUCEVILLE PLANT CALENDAR YEAR 19/1

	<u> </u>	
CODE #	Material Description	
	·	
Chem 1	Vinyl Chloride	
Chem 1	Lauroyl Paroxide	
7	Gelatin	₽-
11		-
25	Styrene Monomer	
20	Butadiene	
27	Potassium Persulfate	—
28	Dodecyl Mercaptan	_
29	Dresinate 200 70%	—
35	Dresinate #731	- .
37	Methocel 65 HG 50 C:S	—
39	Potassium Chloride	
41	Di Vinyl Benzine	
154	Aqua Ammonia	 -
159	Formaldehyde 40%	-
163	Oleic Acid	—
• 166	Potash Caustic Flake	-
175	Triethanolamine	-
197	Silicate of Soda	
228	Tetra Ethanol Ammonia	- .
233	2-Ethyl Hexanol	
1001	Tolucne Sulphonic Acid	┢.
1002	Perchlorethylene	├─ `
1003	Phthalic Anhydride	
1004	Iso-Octyl Alcohol	-
1008	Adipic Acid	 -
1010	Butyl Alcohol	
1015	Tricthylene Glycol	 - .
1016	Stabilizer 13-V-55A	}—
1055	Iso Decyl Alcohol	
1023	Bisphenol "A"	-
1032	Pumaric Acid	-
1033	Maleic Anhyaride	_
1035	Pelargonie Acid	├─ .
1055		
1056	1,3 Butylene Clycol	
1060	Ethylene Clycol	
1061	1,4 Rutanchiol	-
1066	Glycerol	
1072	Thermolite #12	_
1020	Nrosat #16	
1082		
1093		
1091		— .
1105		⊢ ∶
1117		-
1119		-
1120		-
1121		-
1122	Collulose Acetate Butyr	
1124	Ethyl Acetate	===
1125		
1126	Propylene Glycol	
·		
1121	Elannous Chlorido F.M. (Cob Givent Hiend	-
11 <i>E)</i>	s area (tax) the very	

	3144	retra leopropyl Titanat
	-1145	AL fol-1:-10 Al cohol
	1110	DiMethyl Formamide
	11,25	Isopropenul
	1150	Acrawax C
	77(9)	Advawax 140
	1162	Hocehst Wax E
•	1164	Di Iso Butyl Carbinol
	1198	Sympton 160
	2020	T M 918
	2026	Stabilizer 8-V-1
	2042	1,6 Hexanediol
	2013	Iso-butyl Alcohol
	2044	Multrathane 17
-1	2046	S-101 Polyester
•	SO ₁ 1.1	S-102-160 Polyester
	2048	S-103
	2049	S-105 "
•		S106 *
	2050	
	2053	Aldo R. P.
	2056	Al fol 810
	2007	Neopentyl Clycol
	2062	Diethylene Glycol
•	2066	S-1019-75 Polyester
	2069	T-831
	2070	1,2,6 Hexane
	2073	Poly G-1020 P Diol
	2074	Hylene W
	SC(7)	Tin Stabilizer R-037
	2101	Sarkosyl L
•	2104	CO-75 Polyurethane
٠	2114	Tetra Hydro Furan
•	2115	CO-77 Polyurcthane
	2119	MATEL3
	27.55	Poly G 630 P .
	2130	Cab Interm Sol.
-	2142	Cymcl 301
	21/13	Morpholine
	2156	1010 Catalyst
•	2175	1010 Catalyst S-102-70 Polyester
•	2176	S-1015135
	2180	Thermolite T-9
•	21.82	M D I Stearate
-	2183	T D I Stearate
÷	2185	R-109-300 Polyester
<u> </u>	2192	C S Crade Tale
	1133	Stabilizer Symprom 512
MADI	-0	Hater
	1	Revertex
	2	R. Revertex
	20	Neoprene Latex Type
*	64	Remular Concentrate
•	83	Type 2000
	85	Type 1009
	86	Type 2000 L
27	307_	Clay - Ordinary
 -	372	iirflo Super-Cel
DAB	274	Perven #1
<u>ج</u>		
	256_	Emilphor
	259	Mckal BA 75
	27)	Aquarex MDL Paste
	205	Darven #7
	56.(56.k	6955 Cascin
	_ 211/	Marasperse

COLL 632 Gum Arabic 701 Methocel 100 Cpa. 702 Acrylsol G G 709 Methocel 8000 RODE 611 Water Soluble Desdurant VULC 10 Neozone B 20 Zinc Oxide \$15 55 Zenite Special 56 AA-2246 Antioxicent 76 Tetrone A 78 Setzit \$5 83 Arazate (Powler) 85 2,5 Ditertiary Butyl 88 Super fine Flour Sulfur 89 Vandex KEFP 755 Sowieide G PIG 578 Continex S R F 538 Red - 30 696 Darco K B 1334 Vinylized Linting Viole 1362 Black C.F. 1376 Amerba Black 1403 Nuchar C N 1441 Mogul A 1476 Titanox A 168 LO 1529 105 Lakolene Violet SOIL 113 Xylol 131 Methyl Etbyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 878 500 Rlend or 50% Syn 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 8 1005 E10898 1007 Kane Ace B-12 8 1009 Rucon B-22 Resin 1013 GB-5010 Resin 1047 Kurcha BTA III S		1
701 Methocel 100 Cps. 702 Acrylsol G S 709 Methocel 8000 RODE 611 Water Soluble Deadsrant VULC 10 Neozone D 20 Zinc Oxide #15 55 Zenite Special 56 AA-2246 Antioxicent 70 Tetrone A 78 Setit #5 83 Arazate (Powler) 85 2,5 Ditertiary Butyl 88 Super fine Flour Sulfur 89 Vandex KEEP 755 Sowicide G PIG 578 Continex S R F 538 Red - 30 696 Darco K B 1334 Vinylized Linting Viole 1362 Black C.F. 1376 Curerba Rlack 1403 Nuchar C N 1447 Titanox A 168 L0 1529 10% Lakolene-Violet SOIL 113 Xylol 131 Methyl Ethyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 878 500 Rlend or 50% Syn 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E10898 1007 Kane Ace B-12 1009 Rucon B-22 Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S		Nancol N
702 Acrylsol G S 709 Methocel BOOD RODE 611 Water Soluble Decdurant VULC 10 Neozone D 20 Zinc Oxide #15 55 Zenite Special 56 AA-2246 Antioxicent 76 Tetrone A 78 Setsit #5 83 Arazate (Powler) 85 2,5 Ditertiary Butyl 88 Super fine Flour Sulfur 89 Vandex KEEP 755 Sowieide G PIG 578 Continex S R F 538 Red - 30 696 Darco K B 1334 Vinylized Linting Viole 1362 Black C.F. 1376 Superba Black 1403 Nuchar C N 1441 Mogul A 1470 Titanox A 168 LO 1529 10% Lakolene-Violet SOIL 113 Xylol 131 Methyl Etbyl Ketone 4 847 D I O P Flastersizer 568 Experimental Wax Blend 937 Caster Oil 578 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1000 Racon B-22 Rezin 1013 GB-6010 Rezin 1013 GB-6010 Rezin 1013 GB-6010 Rezin 1017 Kurcha BTA III S		
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1376 Carperba Black 1403 Nuchar C N 1441 Mogul A 1476 Titanox A 168 LO 1529 10% Lakolene Violet BOIL 113 Xylol 131 Methyl Ethyl Ketone 8	1334	Vinylized Linting Violet
1403 Nuchar C N 1441 Mogul A 1476 Titanox A 168 LO 1529 10% Lakolene-Violet BOIL 113 Xylol 131 Methyl Ethyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 8YN 500 Rlend or 50% Syn 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 R-28 Ruenn Resin 1013 GB-010 Resin 1013 GB-010 Resin		Black C.F.
1403 Nuchar C N 1441 Mogul A 1476 Titanox A 168 LO 1529 10% Lakolene-Violet BOIL 113 Xylol 131 Methyl Ethyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 8YN 500 Rlend or 50% Syn 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 R-28 Ruenn Resin 1013 GB-010 Resin 1013 GB-010 Resin		
1476 Titanox A 168 LO 1529 10% Lakolene Violet BOIL 113 Xylol 131 Methyl Ethyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil BYN 500 Rlend of 50% Syn 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E10898 1007 Kane Ace B-12 1008 R20 Ruenn Resin 1013 GB-010 Resin 1047 Kurcha BTA III S	1403	Nuchar C N
1529 10% Lakolene-Violet BOIL 113 Xylol 131 Methyl Etbyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 8YM 500 Rlend or 50% Sym 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 Re-20 Ruenn Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S	1441	Mogul A
## BOIL 113 Xylol		Titanox A 168 LO
131 Methyl Ethyl Ketone 8 847 D I O P Plastersizer 8 863 Plasticizer TG-8 868 Experimental Wax Blend 937 Caster Oil 8YM 500 Rlend of 50% Sym 90C 918 Geon 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 R-20 Ruenn Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S	1529	
* 847 D I O P Plastersizer * 863 Plasticizer TG-8 : 868 Experimental Wax Blend 937 Caster Oil 8YM 500 Blend of 50% Sym 90C 918 Geon 121 966 VC - 113 99% Acrylold K-120 N 1000 VC-111 * 1005 E10898 1007 Kane Ace B-12 * 1008 R20 Ruenn Resin * 1009 Ruenn B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S	SOIL 113	Xylol
• 847 D I O P Plastersizer • 863 Plasticizer TG-8 • 868 Experimental Wax Blend 937 Caster Oil 8YM 500 Rlend or 50% Sym 90C 918 Geom 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 • 1005 E10898 1007 Kane Ace B-12 • 1008 R28 Ruenn Resin • 1009 Ruenn B-22 Resin 1013 GB-5010 Resin 1047 Kurcha BTA III S	131	Methyl Etbyl Ketone
• 863 Plasticizer TG-8 - 868 Experimental Wax Blend 937 Caster Oil 8YM 500 Rlend or 50% Sym 90C 918 Geom 121 966 VC - 113 994 Acrylold K-120 N 1000 VC-111 • 1005 E10898 1007 Kane Ace B-12 • 1008 R28 Ruenn Resin • 1009 Ruenn B-22 Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S		D I O P Plastersizer
### 1005 Brown B-22 Resin 1047 Kurcha BTA III S		Plasticizer TG-8
### 500 Rlend of 50% Syn 90C 918 Geon 121 966 WC - 113 994 Acryloid K-120 N 1000 WC-111 1005 E-10898 1007 Kane Ace B-12 1008 B-28 Ricon Resin 1009 Ricon B-22 Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S	868	
918 Geon 121 966 VC - 113 994 Acryloid K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 P-28 Rucon Resin 1009 Rucon B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
918 Geon 121 966 VC - 113 994 Acryloid K-120 N 1000 VC-111 • 1005 E-10898 1007 Kane Ace B-12 • 1008 B-28 Ruean Resin • 1009 Ruean B-22 Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S		
966 VC - 113 994 Acryloid K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 B-28 Rucon Resin 1009 Rucon B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
994 Acrylold K-120 N 1000 VC-111 1005 E-10898 1007 Kane Ace B-12 1008 P-28 Rucon Resin 1009 Rucon B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
1000 VC-111 • 1005 E10898 1007 Kane Ace B-12 • 1008 P28 Ruenn Resin • 1009 Ruenn B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
• 1005 E-10898 1007 Kane Ace B-12 • 1008 R-20 Ruenn Resin • 1009 Ruenn B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
1005 R20 Rueon Resin 1009 Rueon B-22 Resin 1013 GB-0010 Resin 1047 Kurcha BTA III S		
•• 1005	1007	Kane Ace B-12
1009 Rucon B-22 Resin 1013 GB-6010 Resin 1047 Kurcha BTA III S		
1013 GB-6010 Resin 1047 Kurcha BTA III S		
1047 Kurcha BTA III S		
TOTALS		
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RAW MATERIAL REQUIREMENT
HOOKER CHEMICAL/RUCO DIVISION-HICKSVILLE PLANT
CALENDAR YEAR 1972

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Code #	Material Description
Chem 1	Went Chine de Mann
Cuem 1	Vinyl Chloride Mono.
<u> </u>	Trichlorethylene
	Lauroyl Peroxide
	Gelstin
8	Vinyl Acetate
23	Styrene Monomer
	Butadiene
27	Potassium Persulfate
28	Dodecyl Mercaptan
35	Dresinate 731
37	
39	
41	
154	Agua Ammonia
159	Formaldchyde 40%
163	Oleic Acid
166	Potash Caustic Tech.
175	Triethanolomine
197	
228	Tetra Ethanol Ammon
233	2-Ethyl Hexanol
1001	Toluene Sulphonie
1002	
1003	Phthalic Anhydride
1004	Iso-octyl Alcohol
1009	Adipic Acid
1015	Tricthylene Glycol
1016	Dioutyl Timbi laurate
	Neofat Pló
1022	
1023	
1032	Fumaric Acid
1033	:Inleic Anhydride
1035	
	Tri Decyl Alcohol
1050	
. 1061	1,4 Butanediol
1066	
	Methyl Amyl Alcohol
1082	Ricerry Amy Alcohol
1093	
1093	Methyl Caphylate

•
1094 Mothylene 2855
1097 BC-100
1102 Iso-Phthalic Acid
1112 BC - 200 1117 Trimellitic Aphydride
1117 Trimellitic Anhydride 1121 Collosolve Acetate
1122 Cellulose Acetate But
1124 Ethyl Asctate
1125 Toluci
1127 Stannous Chloride
1129 P.M. 3866 Glycol Bl.
1144 Tetraisopropyl Titan,
1145; Alfol. 610 Alcohol 1149; Di Mcthyl Formamide
1152 Isopropanol
1158 Acrawax C
1164 Di-Iso Butyl Carbinol
1170: Mondur S
1181 Topanol CA
1187 Multrathon R-74
1198 Sympton 160
2026 Stabilizer 6-V-1 2042 1.6 Hexandediol
2043 Iso Butyl Alconol
2044 Multrathane M
2046 S-101-55 Polyester
20-7 S-102-160
₹ 2048i 5-103 "
2049: S-105
2050: S-105
2056 Alfol 810
2061 Neopentyl Glycol
2052: Diethylene Glycol
2065 Stabaxol I
2066 Folvester S-1019-75
2074 Hylene W
2053 Mondur- TD 80
2114 Tetra Hydro-Furan
2117 1.4 Cycchexanedimeth. 2140 T-18
2142i Cymel 301
2143 Morpholine
2156 1010 Catalyst
2165; Iso Nonvi Alcohol
2183 T D I Stearate
2166 S-103-35 Polvester
₹ 7191; S-1021-110 Polvester
2192 C S Grade Tale
* 7159 S-502 Polyester

	•
2196	Chemetron Wax 100
2198	Di Ethylamine
# 2200	S-1011-35 Polyester
£ 2201	F-101-60 "
2203	F-101-60
	TMDI
2203	L-45 Silicone
2203	1.6 Hexemethylene
2209	Methyl Collosolve
2211	Myristyl Helene W
2214	Carstan 8
2215	Carstan 18
¥ 2221	R-101-110 Polyester
# 2226	S-105-40 "
# 2227	S-1015-120-220 "
# 2223	XL 2269 L Prepolymer
# 2231	20% M T S A
2233	6vn 60000 1145 C B
	Surjactant 1165 G.E.
# 2237	S-1023-20 Polyester
2239	Recinoleic Acid
# 2244	S-105-75-150 Polvesta
# 2243	S-1021-70-150 "
# 2244	
¥ 224K	S-102-40-150 "
\$ 2249	S-105-55-78 "
¥ 2250	5-102-70-180 "
2256	
2257	N-Propanol
₹ 2273	S-1019-15 & S-1019-55
- 2-44/-	3-1013-13 8 3-1013-33
MAIN	
	•• • • •
a	
11	
21	
20	Neoprene Latex
EX	
307	Clay-Ordinary
372	Hyflo Sper-Cel
DAB	
25 4	Darvan
255	Emulphor
7231	Nekal BA 75
271	Aquarex MDL Paste
	#955 Casein
. 267	
288	Blancol N
COLL	
682	Gum Arabic
	Methocel 100 Cps.
	THE PROPERTY OF THE PROPERTY O

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		_
702	Acrylsol G S .	122
708	Ludox Calleidal Sill.	122 36,912
709	Methocel 8000	17
RODE		
	Water Soluble Deod.	13
		! i
VULC		
	Neozone D	1 1
70	French Proces Zine O.	346
	Zenite Special	60
		135
		122
	Aranate (Powder)	21
	2.5 Ditertiary Btuvl	33
	Super Fine Flour Sul.	119
		17
07	VEHUCX	H 1/
MATN		
MAIN	Type 2000 L (A-49)	774 507
		714.587
₹ 100	Type 1009 (A-64)	616,140
		
KEEP	م دفعہ م	
/35	Sowicide G.	50
PIG		
578	Continex S R F	126
578 588	Red-30	82
578 588 696	Red-30 Darco k B	82 27,219
578 588 696 1362	Red-30 Darco k B Black C F	82 27,219 699
578 388 696 1362	Red-30 Darco k B Black C F Superba Black	82 27.219 699 12.600
578 588 696 1362 1376 1403	Red-30 Darco k B Black C F Superba Black Nuchar C N	82 27,219 699 12,600 24,915
578 588 696 1362 1376 1403	Red-30 Darco k B Black C F Superba Black Nuchar C N Yogul A	82 27,219 699 12,600 24,915 7,380
578 588 696 1362 1376 1403	Red-30 Darco k B Black C F Superba Black Nuchar C N Yogul A	82 27,219 699 12,600 24,915
578 588 696 1362 1376 1403 1441	Red-30 Darco k B Black C F Superba Black Kuchsr C N Yogul A Titanox A 158-LO	82 27,219 699 12,600 24,915 7,380
578 588 696 1362 1376 1403 1441	Red-30 Darco k B Black C F Superba Black Kuchsr C N Yogul A Titanox A 158-LO	82 27,219 699 12,600 24,915 7,380 127
578 588 696 1362 1376 1403 1441 1476 SOIL	Red-30 Darco k B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO	82 27,219 699 12,600 24,915 7,380 127
578 588 696 1362 1376 1403 1441 1476 SOIL 113	Red-30 Darco & B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411
578 588 696 1362 1376 1403 1441 1476 SOIL 1131 866	Red-30 Darco & B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411
578 588 696 1362 1376 1403 1441 1476 SOIL 113 131 866 886	Red-30 Darco k B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411
578 588 696 1362 1376 1403 1441 1476 SOIL 1131 866	Red-30 Darco & B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411
\$78 \$88 696 1362 1376 1403 1441 1476 \$01L 113 131 866 886 937	Red-30 Darco k B Black C F Superba Black Nuchar C N Yogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411
\$78 \$88 696 1362 1376 1441 1476 \$01L 113 131 868 886 937	Red-30 Darco k B Black C F Superba Black Nuchar C N Fogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411 179 150
\$78 \$88 696 1362 1376 1441 1476 \$01L \$131 868 886 886 937	Red-30 Darco k B Black C F Superba Black Nuchar C N Kogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil Hercolyn	37,662 452,411 10,634
\$78 \$88 696 1362 1376 1441 1476 \$01L \$131 868 886 886 937	Red-30 Darco k B Black C F Superba Black Nuchar C N Kogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil Hercolyn	37,662 452,411 10,634
578 588 696 1362 1376 1441 1476 SOIL 113 131 866 886 937 5YN 424 463	Red-30 Darco k B Black C F Superba Black Nuchar C N Mogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Percolex G-62 Caster Oil Hercolyn VYHH Resin	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411 179 150 9
578 588 696 1362 1376 1403 1441 1476 SOIL 113 866 886 937 \$YN 424 463	Red-30 Darco k B Black C F Superba Black Nuchar C N Frogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil Hercolyn VYHH Resin Pent. A Sol IRS75xA C-155	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411 179 150 9
578 588 696 1362 1376 1403 1441 1476 SOIL 113 866 886 937 \$YN 424 463	Red-30 Darco k B Black C F Superba Black Nuchar C N Mogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil Hercolyn VYHH Resin Pent. A Sol IRS75xA C-155	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411 177 150 9 10,634 4,525 42,524 3,663,040
578 588 696 1362 1376 1403 1441 1476 SOIL 113 866 886 937 5YN 424 463 900 \$500	Red-30 Darco k B Black C F Superba Black Nuchar C N Frogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Paraplex G-02 Caster Oil Hercolyn VYHH Resin Pent. A Sol IRS75xA C-155 VC-111	37,662 452,411 10,634 4,525 42,544 363,040 43,920
578 588 696 1362 1376 1403 1441 1476 SOIL 113 131 868 886 937 5YN 424 463 900 4 550 1005	Red-30 Darco k B Black C F Superba Black Nuchar C N Frogul A Titanox A 158-LO Xylol Methyl Ethyl Ketone Experimental Wax Bld Peraplex G-62 Caster Oil Hercolyn VYHH Resin Pent. A Sol IRS75xA C-155 VC-111 E-1068S-1	82 27,219 699 12,600 24,915 7,380 127 37,662 452,411 177 150 9 10,634 4,525 42,524 3,663,040

RAW MATERIAL REQUIREMENT HOOKER CHEMICAL/RUCO DIVISION-HICKSVILLE PLANT CALENDAR YEAR 1973

CODE #	MATERIAL DESCRIPTION
Chem 1	Vinyl Chloride
2	Trichlorethylene
5	Leuroyl Peroxide
7	Gelatin
8	Vinyl Acetate
25	Styrene
26	Butadiene
27	Potessium Persulfate
28	Dodecyl Mercaptan
29	Dresinate #208 70%
35	Dresinate #731 (70%)
37	Methocel 65 PG-50
39 41	Potassium Chloride
	Divinyl Brazene -
46	Dresinate #731 18% Soli Dresinate #208 18% Soli
48	Dresinate #208 18% Sol
154	Agua Ammonia
159	Formaldchyde 40%
163	Oleic Acid
166	Potash Caustic Tech.
173	Triethanolamine
228	Tetra Ethanol Ammonia
233	2-Ethyl Hexanol **
1001	Toluene Sulphonic
1002	Perchlorethylone
1003	Phthalic Anhydride
1004	Iso-Octvl Alcohol
1008	Adipic Acid
1010	Butyl Alcohol
1014	Caprylic Acid
1015	Triethylene Glycol
1016	Dibutyl TinDi Laurate
1022	Iso-Decvl Alcohol xxx
1023	Iso-Decvi Alcohol ***
1032	Funaric Acid
1033	Maleic Anhydride
1035	Pelarronic Acid
1040	Neofat 18-59

	•
1055	Tri Decyl Alcohol
1056	1.3 Butvlene Glycol
1060	Ethylene Glycol
1061	1,4 Eutanediol
1006	Glycerol
1072 1032	r-12
1093	Eicarbonate of Soda Hethylene #2208
1094	Methylene #2855
1097	BC-100
1102	Iso-Phthalic Acid
1112	BC-200
1117	Trimellitic Anhydride
1118	Emery #144
1124	Etnyl Acetate
1125	Toluol Propylene Glycol
1127	Strnnous Chloride
1129	PK 3066 Glycol Blend
1133	Sympron 512
1144	Tetraisopropyl Titanary
1145	Alfol-610 Alcohol
1149	Di Methyl Formamide
1152	Isopropenol
1164	Di-Iso Butyl Carbinol
1181 2042	Topanol C A 1,6 Hexandediol
2042	Iso Butyl Alcohol
2044	Fultrathane M
* 2046	S-101-55 Polyester
* 2047	S-102-160 "
* 2048	S-103-90 "
* 2049	5-105-120
* 2050	s-106-35 "
2061	Neopentyl Glycol
2062	Diethylene Glycol Stabaxol I
* 2066	Polyester S-1019-75
2073	Poly G 1020-P
2074	Hylene W
2063	Mondur TD 80
2114	Tetra Hydro-Furan
* 2115	CO-77 Urctaine Sol.
2117	1,4 Cycchexanedimeth.
. 2121	10% Formalaehyde
2122	Poly 6 630
	Alfol #6 C-10-12 Alcohol
2126	Cymel 301
. 2142	CAMET ANY

± 2159	S-502 Polyester
2180	Thermolite T-9
2163	1111 >510
<u> </u>	Thi Stearate
2192	S-103-35 Polyester
	C S Grade Tale Chemetron Wax 100
2196	Gremetron Wax 100
21 48	Di Ethylamine
* 2700	S-1011-35 Polyester
± 2701	F-101-60 "
2206	L-45 Silicone
2208	1.6 Hexamethylene
2209	Methyl Callosolve
2211	Myristyl Holene W
2214	Carstan 8
2215	Carstan 18
+ 2218	
★ 2226	Iso-Phorone Di-iso. S-105-40 Polvester
¥ 2227	S-1015-120-220 "
	3-1013-120-220
* 2231	20% M T S A
2242	S-105-75-150 Polyester
* 2243	S-1021-70-150
* 2244	5-1019-75-200 "
* 2247	S-101-55-150 "
₩ 2248	S-102-40-150
* 2250	S-102-70-120 "
2237	N-Proponol
★ 2275	S-105-40-57 Polvester
2296	Chemetron Wax 100
2298	Moca
2299	30% AND-MSA Cat.
= 2319	S-1022-20 Polyester
2320	1sophone Diamine
	C. 1014 if B
	S-1019-25 Polyester
2348	45% EAB 381.5 Lace.
* 2349	S-103-25 Polyester
MAIN O	Water
1	Revertex 73%
2	60% Natural Latex
20	Neoprene Latex
* 101	Type 2000-53 (A-74)
* 102	Type 1009 (A-77)
# 104	Type 2000 (A-79)
EX 372	Hv Flo Super Cel
Din 254	Perven #1
256	Emulphor-on-670
259	Nekal BA 75
271	ACHIATEN MOL Paste
4/1	Senates unr Laste

HKR 001 C

286	₹95 Casein
COLL	
682	Gum Arabic .
701	Methocel 100 Cps.
702	Acrysol G. S.
709	
709	Methocel-8000
RODE	
611	Water Soluble Deod.
	water soldsie bedd.
VULC	<u></u> -
10	Neozone D
20	French Proces Zinc O.
55	Zenite Special
56	AA-2246 Antioxident
76	Tetrone A
83	Aranate (Powder)
85	2.5 Ditertiary Btuyl.
- 83	Super Fine Flour Sul.
89	Vandex
KEEP	
755	Dowicide G.
	DOWNERS OF
PIG	
578	Continex S R F
558	Red-30
696	Darco K B
1423	Nuchar C N
1276	Titanox A 168-LO
	12 (1110 11 100 20
SOIL	
113	Xvlol
131	Methyl Ethyl Ketone
868	Experimental Wax Ald.
£86	Paranlex G-62
929	E P O
937	Caster Oil
SYN	
424	Hereplyn D
463	VYHM Resin
900	Pentatyn A
· * 1065	E-10658-1



HOOKER CHEMICAL PUCD DIVISION-CHEMICAL BUSINESS AREA CALENDAR YEAR 1974

CODE	NATERIAL DESCRIPTION
Chen 1	Vinyl Chloride
	Trichlorethylene
3	Lauroyl Peroxide
7	Gelatin
R	Vinyl Acctate
37	Methocol 65 PG-50
175	Tricthanolamine
233	2-Ethyl Hexanol
1001	Tolurne Sulphonic Acid
1002	Perchlorethylene
1003	Phthalic Anhydride
1004	Iso-Octvi Alcohol
1008	Adipic Acid
1015	Tricthylene Glycol
1015	Dibutyl Tin Di Lourate
	Isn-Decyl Alcohol
1023	Eisphenol "A"
1033	Maleic Anhydride
1035	Pelarnonie Acid -
1035	Tri Decyl Alcohol
1056	1.3 Butylene Glycol
10e0	Ethylane Glycol
1061	1,4 Butsnediol
1056	Glycerol
1082	Bicarbonate of Soda
1093	Hethylone #2208
1094	Methylene #2209
1097	BC-100
1102	lso-Phthelic Acid
1117	Triwellitic Anhydride
1113	Emery #144
1125	Toluc!
1125	Francismo Giveol
1127	Stannour Chloride
1129	PM 3336 Giveol Blend
1144	Tetraisopronyl Titanate
1145	Aliel-610 Alcohol -
1149	Di Methyl Formanide
1152	Isopropenol
1164	Di-Iro Eutyl Carbinol
1181	Topenal C A
1101	TOREROL O A

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	2319 +	S-1022-20 Polyerter
	2320	Isophone Diamine
	2322 =	S-102-1.7-185
	2334 +	5-105-75
	2343	Irranox 107%
	23/6 *	S-101y-23-35
	234% ±	454 FAR Sol.
	2349 *	S-103-25
	2350 *	S-1017-25
	2352 *	S-1023-40-105
<u>. </u>	2359	Cymel 370
	2360 ± 2362 ±	S-105-40-118
	2365 ×	B-270-L Propol Dabco (Solid)
	2366	Silicone L-540
	2367 *	S-1011-55
	2378	Succinic Anhydride
	2352	Harkure UL-6
	2391	Monday E-320
	2393 *	S-1019-120-230
	2395 *	S-105-75-167
	2396	N-Methyl Ethanolamine
	2403	Iscnate 125-M
	2404	Freen TF
	2403 *	CO B 3436 L H Prepol .
	2415 *	Rucoflex BD-1
	2416 *	Rucorlex F-1201
MAIN		Water
EX	372	Celite (Hyflow Super-cel)
COLL	306	H I I I I I I I I I I I I I I I I I I I
COLL	708	Ludox "AS"
PIG	695	3000 V 8
F16	1403	Darco K B
	1576	Ruchar C N Pirment A
	1376	Present A
SOIL	113	Xvlol
2012	131	Methyl Ethyl Kotone -
	658	Paraplex G-62
		- Brance G- OZ
SYN	463	Villi Resin
		·····



RAW MATERIAL REQUIREMENT HOOKER CHEMICAL RUCO DIVISION-CHEMICAL BUSINESS AREA CALENIAR YEAR 1975

CODE	MATERIAL DESCRIPTION	
Chem 1	Vinyl Chloride	<u>-</u> -
3	Trichlorethylene	
	Laurovi Peroxide	□ .
7	Gelatin	
8	Vinyl Acetace	1
37	Mathocal F-50	
175	Triethanolamine	_}
233	2-Ethyl Hexanol	
1001	Toluene Sulphonic Acid	
1002	Parchlorethylane	4
1003	Phonelic Anhydride	_
1004	Isn-Octvl Alcohol	·
1003	Adipic Acid	_ -
1125	Pronvlene Glycol	
1016	Dibutyl Tin Di Laurate	
1022	Iso-Decvl Alcohol	
1023	Bishhenal A	
1033	Maleic Anhydride	-
1055	Tri-Decyl Alcohol	
1056	1.3 Butylene Glycol	 - → •
1060	Ethylene Glycol	
1061	1,4 Butanediol	
1066	Glycerol	
1082	Bicarbonate of Soda	- -↓
1097	BC-100	- } ·
1102	Iso-Phthalic Acid	<u> </u>
1117	Trimellitic Anhydride	
1124	Ethvi Acetate	
1123	Toluol	
1127	Stannous Chloride	<u>_</u> _i
1129	PM 3866 Glycol Blend	
1144	letra Isopronyl Titanate	
1145	Alfol #610	 ,
1129	Di Methyl Formamide	<u>;</u>
115?	langenenel	l
1164	Di-Iso Butvl Carbinal	_1
1161	lonanol CA	
2021	Hoechst Wax OP	
2042	1,6 Hemandediol	1
2043	Iso Butyl Alcohol	

2044	Multrathane M
2946 ×	S-101-55 Polyester
2047 *	S-102-160 "
201.8 *	S-103-90
2049 #	s-105-120 "
2050 *	S-106-35 "
2056	Alfol &10
2061	Neopentyl Glycol
2062	Diethylene Glycol
2065	Stabaxol I
2074	Hylene W
2083	Mondur TD 80
2114	Tetra livero-furan
2117 2122	1,4 Cycohexanedimethanol 201y C-h30
2142	Cyme) 301
2185 ¥	R-109-300
2363 ×	F-102-50 Polvester
2196	Chemetron Wax 100
2198	Di Ethylamine
2200 ×	S-1011-35 Polyester
2206	L-45 Silicone
2205	1.6 Bexamethylene
2209	Hethyl Cellosolve
2211	Myrstyl Helene W
2214	Carstan 8
2218	Iso-Phorone Di-Isocvante
2226 *	S-105-40 Polyester
2227 *	5-1015-120-220 Polyester
2242 *	S-105-75-150 Polyester
2243 *	S-1021-70-150 "
2248 *	S-102-40-150 (305-183)
2250 *	S-102-70-180 Polvester
2257	N-Propanol ·
2273 ×	S-1019-75-150 Polyester
2296 *	S-102-55-305 30% AMP-MSA Cat.
2299 *	30% AMP-MSA Cat.
2300	EAS-301-5
2320	Isophone Diamine
	S-102-37-185 Polyester
2330	EC 2690 Merhane Sul. Acid
2331 2332	AMP (Romijar)
2334 *	Di Bromo Buteneciol S-105-75 Polyester
2334 -	Jenesey 1075
· 2343	Irganox 1076 S-1019-25-35 Polyester
2348 ×	45% HAB Sol.
2352 *	5-1023-40-106 Polvester
2359	Cymel 370
2360 *	S-105-40-118 Polyester
2300	<u> </u>

- 3 -

** !	•	
	2458	Irranox #1035
	2460	lono
	2462 ¥	F-1403 Polyester
	2467 ×	F-1016
	2468 ×	:- 1022-115 Polyester
	2400	Stannous Oralate E
	2470	Deruser OK 412
	2472	N-3936-L Prenol
	2473	Tucch 20 i
	2474	Tritonx 405
	2475	Emilsifier Solution
	2476	Sodium Hyroxide
	2477	Acrysol ASE-75
	2478	14% H M D A
	2479	Thickener Solution
	2481	20% Sodium Hvd: xide
	2482 *	S-1019-55 Polycater
EX	372	Celite (Hvflow Super-cel)
PIG	1577	Polyection C
	1593	Nuchar C-Ell-N
	1594	Activated Carbon C n
SOII		Xvlol
	131	Mothvi Ethyl Ketone
	886	Peraplex G-62
אys	463	VYHH Resin
		\;
MAIN	1 0	Water

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HOOKER CHEMICAL/RUCO D/VISTON-CHEMICAL BUSINESS AREA CALENDAR YEAR 1976

CODE	MATERIAL DESCRIPTION
Chem 233	2-Ethvl Hexanol
1001	Toluthe Sulphonic Acid
1002	Perchlorethyleae
1003	Phtnalic Annydride
1004	Iso-Cctyl Alcohol
100έ	AdipicAcid
1014	Caprylic Acid
1015	Tricthylene Glycol
1016	Dibutyl Tin Di Lourate
1022	Iso-Decyl Alcohol
1023	Bischenel A
1033	Maleic Annydride
1035	Emtac #1202 Tri-Decyl Alcohol
1055	1.3 Butylene Glycol
10é0	
1051	Ethylene Glycol 1.4 Butanediol
1066	Glycerol
1082	
1094	Bicarbonate of Soda
1094	Methylene 2209
1102	BC-100 Iso-Phthalic Acid
1117	Trimellitic Anhydride
1124	Ethyl Acetate
1125	Toluol
1126	Pronvlene Glycol
1127	Stannous Chloride
1129	Giveni Blend Pm 3866
1127	Tetra Isonropyl Titanate
1145	Alfol #510
1145	Di Methyl Formamide
1152	Isorococol
2042	1,6 Hexandediol
2043	Iso Eutyl Alcohol
· 2044	Multrathane M
2046 *	S-101-55 Folvester
20/:7 ×	S-102-160 Polyester
2049 ±	S-105-120
2021	Rocchst Wax

•	•
2050 *	S-106-35
2061	Neggentyl Glycol
2062	Dicthylene Glycol
2065	Stabasol I
2073	Polv G-1020 P
2074	Hylene U
2080	Di-Propylene Glycol
2083	Mondur TD 80
2114	Tetra Hydro-Furan
2117	1, /: Cycohexanedimethanol
2122	Poly G-630
2128	1,1,1 Trichlorethane
2142	Cymcl 301
2159 *	F-109-60 Polvester
2195	Chemetron Wax 100
2198	Di Ethylemine
2206	L-45 Silicone
2208	1.6 Hexamethylene
2209	Methyl Collosolve
2211	Myrstyl Helche W
2214	Cerstan 8
2218	Iso-Phorone Di-Isocvante
2226 *	S-105-40 Polyester
2227 *	S-1015-120-220 Polyester
2242 *	S-105-75-150 Polvester f
2243 *	S-1021-70-150 Polyester
2250 ×	S-132-70-180 Polyester
2257	N-Propanol
2276 *	S-1015-80 Polvester
2281 *	S-1021-75 Polyester
2296 ×	S-102-55-305
2299 ¥	30% AMP-MSA Cat.
2320	Isophone Diamine
2322 *	S-102-87-145 Polvester
2330	EC 2590 Nethane Sul. Acid
2331	ANP (Perular)
2334 *	S-105-75 Folvester
2343	Irranox 1076
2349 *	5-103-25 Polvester
2359	Cymel 370
2360 *	S-105-40-11S Polyester
2367 *	S-S-1011-55 Polvester
2393 ×	S-1019-120-280
2395 *	5-105-75-167 Polvester
2417 *	S-1022-35 Polyester
2431 =	S-102-55 Polvester
5772 #	S-102-110 Polyester
2450	CAB 301-2
2456	Polymer #1000
2457	Tituvin #328

hooker AUCO oivision

PHONE (516) 931-8100 TWX 510 221-1871

May 6, 1975

Mr. John F. Welsch Supervisor of Industrial Waste Bureau of Water Pollution Control Nassau County Department of Health 240 Old Country Road Mineola, N.Y. 11501

Dear John:

Attached are 3 (three) completed copies of the new application form "D" for SPDES permit.

Please refer to our correspondence of April 22, 1975 on the old SPDES form. Outfall numbers 001 and 002 no longer exist. (Hence 003-005 are renumbered 001-003). In the interum the decision was made to close this plant for PVC production. There are no plans to produce another product instead. However, if in the future and alternative product with a water discharge is made we will contact your office.

We feel the Hicksville Site is now in compliance with the water discharge regulations. Per our discussion today (May 6, 1975) discharges 001 to 003 do not require additional treatment. The incinerator for the esterification discharge has been running for several weeks, but with some problems. We expect them to be solved with-in 2 - 4 weeks and this discharge eliminated.

If you have any questions please do not hesitate to call.

Very truly yours,

Malcolm K / Sour

Professional Engineer

HKR 001 03

PLICATION FORM "D" FOR A STATE POLLUTANT DISCHARGE ELIMINATION SYSTEM (SPDES) PERMIT (Becomes A SPDES Permit When Signed By Permit Issuing Official)

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APPENDIX 2
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Page ____ of _ PROJECT OCCIDENTAL Chercy SITE Hooker/12000 COLLECTED BY (Signature) SAM ID NO. (for lab use only) FIELD SAMPLE I.D. REMARKS SAMPLE MATRIX DATE/TIME Soil . 53030\$6001A1 10/5 0900 50:4 10/5 0940 5 304 OG COR AL Soil X 1dx 1055 5355A7 COL AL X 50:6 10/5 1120 5306 07 102 AL Sil 10/5 1400 530709-01A1 RELINQUISHED BY: REMARKS DATE TIME 10/5/1930 DATE TIME RELINQUISHED BY: RECEIVED BY: DATE TIME RECEIVED BY: DATE | TIME | RELINQUISHED BY: DATE TIME The supers 10/5 1830 11/2 311) # 35074RD 3507470212 LAB USE ONLY DATE TIME AIRBILL NO. RECEIVED FOR LABORATORY BY. OPENED BY: DATE TIME TEMPACE SEAL # CONDITION REMARKS

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